

# MINOR NEW SOURCE REVIEW AND BEST AVAILABLE CONTROL TECHNOLOGY (BACT) ANALYSIS PELLET COOLER #1 MODIFICATION FOR MOUNTAIRE FARMS OF DELAWARE, INC.

# 29106 JOHN J. WILLIAMS HIGHWAY MILLSBORO, DELAWARE

OCTOBER 2018

Prepared for:

State of Delaware
Department of Natural Resources
and Environmental Control
Division of Air Quality
100 West Water Street, Suite 6A
Dover, Delaware 19904

On behalf of:

Mountaire Farms of Delaware, Inc. 29106 John J. Williams Highway Millsboro, Delaware 19966

Prepared by:

Duffield Associates, Inc. 5400 Limestone Road Wilmington, Delaware 19808

Project No. 12032.EA



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#### 1.0 INTRODUCTION

Mountaire Farms of Delaware, Inc. is proposing to replace Pellet Cooler #1 at its feed mill located at 29106 John J. Williams Highway in Millsboro, Delaware (see Figure 1). The replacement pellet cooler, like the existing one, will emit particulate matter (PM), including PM less than or equal to 10 micrometers in aerodynamic diameter (PM<sub>10</sub>) and PM less than or equal to 2.5 micrometers in aerodynamic diameter (PM<sub>2.5</sub>). Emission of these pollutants to the atmosphere will continue to be reduced and controlled by an existing cyclone dust collector. However, the applicant is obligated to demonstrate that the existing dust collector qualifies as Best Available Control Technology (BACT).

A modification to the construction permit for Pellet Cooler #1 was previously submitted in July of 2018 (see Attachment 1), which included Forms AQM-1, AQM-2, AQM-3.13, and AQM-5. Some of those forms will be referenced in this BACT analysis. The current pellet cooler control technology is in attainment or not listed for the National Ambient Air Quality Standards (NAAQS) and is considered a minor new source.

In Chapter 7, Part 1125, Delaware Administrative Code [DE Admin. Code]), the Delaware Department of Natural Resources and Environmental Control (DNREC) has adopted the Federal Environmental Protection Agency (EPA) rules pertaining to Prevention of Significant Deterioration (PSD) as contained in Chapter 40, Part 52.21, Code of Federal Regulations (40 CFR 52.21). Section 3.0 of this report provides a detailed review of applicable EPA and DNREC requirements for permitting of the Pellet Cooler #1 modification.

#### 2.0 DESCRIPTION OF PROPOSED FEED MILL MODIFICATION

#### 2.1 FEED MILL MODIFICATION DESCRIPTION

As discussed in Section 1.0, the facility is located at 29106 John J. Williams Highway in Millsboro, Delaware. A diagram of the general process of the feed mill is provided in Attachment 2. Mountaire Farms of Delaware, Inc. plans to replace existing Pellet Cooler #1 with a Hayes & Stolz pellet cooler. The existing cyclone dust collector will not be replaced.

#### 2.2 PROCESS DESCRIPTION

The pellet cooling process takes place after the feed material (consisting of corn, wheat, and soybeans) has been dried in the drying drum, ground into meal, sent to the meal collector, and then sent to Pellet Mill #1 where feed pellets are formed. From Pellet Mill #1, the pellets are conveyed pneumatically to Pellet Cooler #1 where additional air is drawn into the device to cool the pellets. The cyclone dust collector for Pellet Cooler #1 is used to separate entrained fines (PM) in the cooler exhaust air and to collect pellets that incidentally exit the cooler in the exhaust air stream. In the cyclone, fine particulates are separated from the air stream and sent with the pellets to the finished feed area. For a general schematic of the operation of Pellet Cooler #1, see Attachment 2.



#### 3.0 CONTROL TECHNOLOGY ANALYSES

The proposed modification to the pellet cooling process is subject to BACT analysis as part of complying with minor new source review requirements of 7 DE Admin. Code 1125. In this case, those requirements pertain to PM<sub>2.5</sub> that have potential to have emitted rates equal to or greater than 5 tons per year (tpy). The maximum rate of PM generated by the pellet cooler is 50 tons per hour, which is equivalent to 438,000 tpy. The current pellet cooler is being replaced with a Hayes & Stolz pellet cooler. The existing Koger-Air model 2H54 High Efficiency Cyclone will remain and continue to treat emissions from the replacement pellet cooler. Emissions for the control technology equipment are expected to remain the same. Elements of the pellet cooling process located upstream are expected to remain the same.

#### 3.1 BEST AVAILABLE CONTROL TECHNOLOGY

#### 3.1.1 POLLUTANT APPLICABILITY

BACT is required for facilities in Delaware when potential emissions from new emission sources exceed 5 tpy in accordance with 7 DE Admin. Code 1125. In this instance, the replacement of the source equipment, a pellet cooler, triggers the requirement to review the effectiveness of the associated emission control equipment, a cyclone. The pollutants subject to the BACT analysis are PM<sub>2.5</sub>.

#### 3.1.2 METHODOLOGY

BACT is defined in 7 DE Admin. Code 1125 Section 1.9, as:

"...an emissions limitation (including a visible emissions standard) based on the maximum degree of reduction for each pollutant subject to regulation under CAA [Clean Air Act] which would be emitted from any proposed major stationary source or major modification which the Department, on a case-by-case basis, takes into account energy, environmental, and economic impacts and other costs, determines is achievable for such source or modification through application of production processes or available methods, systems, and techniques, including fuel cleaning or treatment or innovative fuel combustion techniques for control of such pollutant. In no event shall application of best available control technology result in emissions of any pollutant which would exceed the emissions allowed by any applicable standard under 7 DE Admin. Code 1120 and 1121. If the Department determines that technological or economic limitations on the application of measurement methodology to a particular emissions unit would make the imposition of an emissions standard infeasible, a design, equipment, work practice, operational standard, or combination thereof, may be prescribed instead to satisfy the requirement for the application of best available control technology. Such standard shall, to the degree possible, set forth the emissions reduction achievable by implementation of such design, equipment, work practice or operation, and shall provide for compliance by means which achieve equivalent results."



This BACT analysis has been performed in accordance with Section 4.3.1.4 of the Delaware Division of Air Quality 7 Delaware Admin Code 1125 which states that emission control technology will be approved by the Department on a case-by-case basis.

The first step in the BACT analysis procedure is the identification of available control technologies. Alternatives considered include controls applied to similar types of sources, innovative control technologies, other pollution prevention measures, modifications of the process or process equipment, and combinations of these measures. The available control technologies are then listed in descending order of air pollution control effectiveness.

Following the identification and listing of available control technologies, the next step in the analysis is to propose the most effective technology on the list generated for approval by the Department or to determine which technologies may be infeasible technically. The third step in the BACT analysis process is to submit the control technology proposed to be installed and operated, the list generated, and any demonstrations to the Department as part of the application. The following sources were used as guidance for determining alternative control technologies and also in determining feasibility:

- Environmental Protection Agency Compilation of Air Pollutant Emissions Factors (EPA AP-42, 2003), Section 9.9.1.1.5 for Animal Feed Mills;
- Previous Permit Modification Application for Pellet Cooler #1 (Mountaire Farms of Delaware, Inc., July 2018)
- DE 7 Admin Code 1125, Section 4.3.1.4 (DNREC, 2016)
- Aircon Corporation Website, <a href="https://aircon-corporation.com/cyclones/">https://aircon-corporation.com/cyclones/</a>
- Matching product to cooling process (Bortone, Eugenio), Feed Pelleting Reference Guide: Section 3: Manufacturing Considerations, Chapter 12: Matching Product to Cooling Processes.

The final step is to select a BACT emissions limitation corresponding to the most stringent, technically feasible control technology that was not eliminated based on adverse energy, environmental, or economic grounds.

#### 3.1.3 BACT ANALYSIS FOR PM/PM<sub>10</sub>/PM<sub>2.5</sub> FROM COOLING PROCESS

Operation of the replacement pellet cooler will be a source of PM emissions. This section details the BACT analysis of the pellet cooler control technologies available.

#### 3.1.3.1 Potential Control Technologies for Pellet Cooler PM Control

The current control technology for Pellet Cooler #1 is a pellet cooler cyclone that will remain after replacement of the pellet cooler. There are two types of pellet cooler cyclones: cyclone and high efficiency cyclone.

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Duffield's literary review did not find additional methods of controlling PM emissions generated during pellet cooling processes. Aircon Corporation states that high efficiency cyclones generally are used in feed mills on pellet coolers, and that they are 'essential in this process as they separate the contaminated hot air from the cooler to the atmosphere'. In an article titled *Matching product to cooling process*, the cyclone control technology is mentioned when talking about the air speed through the pellet cooler which allows for fines to be blown through the cyclone (Bortone, et.al.). According to the Environmental Protection Agency Compilation of Air Pollutant Emissions Factors (EPA AP-42), both cyclones and high efficiency cyclones typically are used in the pellet cooling process (Attachment 3). No additional control technologies were mentioned. The EPA RACT/BACT/LAER Clearinghouse (RBLC) database does not have the cyclone or other pellet cooler control technologies listed on the database. Based on the literary review, Duffield determined the following list of available control technologies in descending order of air pollution control effectiveness:

- High efficiency cyclone; and
- Cyclone

The cyclone emits a weight of 0.36 pounds of total filterable PM per ton of grain throughput while the high efficiency cyclone emits a weight of 0.15 pounds of total filterable PM per ton of grain throughput (see Attachment 3, Table 9.9.1-2 Particulate Emission Factors for Grain Processing Facilities). The high efficiency cyclone releases less PM to the atmosphere.

In this case, the existing control technology for the pellet cooler is a high efficiency cyclone which is the most effective control technology. Since the existing control technology is also the BACT, a demonstration of infeasibility based on the criteria in subsection 4.3.1.4.3.1 through subsection 4.3.1.4.3.4 is not required.

#### 3.1.3.4 Proposed PM/PM10/PM2.5 BACT Emissions Limit for Pellet Cooler

A summary of the PM/PM<sub>10</sub>/PM<sub>2.5</sub> BACT emissions for the current high efficiency cyclone is provided in Table 1 below. Because the existing high efficiency cyclone will remain after replacement of Pellet Cooler #1, the emissions will also remain the same. The Controlled Potential to Emit (PTE) in Table 1 below represents the BACT emission limitations.



Table 1

High Efficiency Cyclone Emissions							
Pollutant	Pollutant Emission Hourly Potential to Permitted Emissions						
	Factor (#/ton) <sup>2</sup>		Emit (PTE)	(tons/year) <sup>1</sup>			
		(lb/hour)	(tons/year) <sup>3</sup>				
PM	0.15	7.50	32.85	32.76			
PM-10	0.075	3.75	16.425	16.38			

#### Notes:

- 1. The Permitted Emissions (tons/year) are the proposed emission limits for PM and PM-10.
- 2. The Emission Factor is based on Table 9.9.1-2 Particulate Emission Factors for Grain Processing Facilities. The PM-10 emission factor is used as a surrogate emission factor for PM-2.5.
- PTE is based on calculations found in the previously submitted Application to Construct, Operate, or Modify Stationary Sources (July 2018).

# 3.2 SUMMARY OF PROPOSED EMISSIONS LIMITATIONS AND DEMONSTRATION OF COMPLIANCE

The high efficiency cyclone is the BACT and will comply with the BACT emission limitations described above. The maximum rate of PM-10 generated by the pellet cooler is 50 tons per hour which is equivalent to PTE of 16.425 tpy. The existing high efficiency cyclone will remain after replacement of Pellet Cooler #1. Emissions are expected to remain the same. Initial and annual documentation of annual operating conditions will be used to demonstrate compliance with the anticipated permit conditions.

12032EA.1018-Mountaire BACT Analysis.RPT.doc



## **ATTACHMENT 1**

PREVIOUSLY-SUBMITTED APPLICATION TO CONSTRUCT, OPERATE, OR MODIFY STATIONARY SOURCES (JULY 2018)



July 18, 2018

Ms. Melanie Smith State of Delaware – DNREC Division of Air Quality 100 West Water Street, Suite 6A Dover DE 19904

Re: Mountaire Farms of Delaware, Inc.

APC-2014/0090-OPERATION Amendment

Dear Ms. Smith:

Enclosed please find the application forms for a modification to the current construction permit for pellet cooler #1 (EU 54). The forms attached as requested are; AQM-1, AQM-2, AQM-3.13, and AQM-5, in addition with a calculation sheet for emission release of PM-10.

The forms attached are for a modification to our current permit where we are seeking to replace the current CP pellet cooler with a Hayes & Stolz pellet cooler. There will; however, be no change to emissions of PM-10 or the production of 50 tons per hour of said equipment.

Should you have any questions, please do not hesitate to call me at 302-934-3070.

Sincerely,

Austin Pajda

Environmental Manager

cc: Tanya Rogers-Vickers (Mountaire)

JR Lapearl (Mountaire)



Form AQM-1 Page 1 of 4

#### Administrative Information

One original and one copy of All Application Forms Should Be Mailed To:
Division of Air Quality
100 West Water Street, Suite 6A
Dover, DE 19904

All Checks Should Be Made Payable To: State of Delaware

Company and Site Information				
1.	Company Name: Mountaire Farms of D	elaware, Inc.		
2.	Company Mailing Address: PO Box 1320	)		
	City: Millsboro	State: <b>Delaware</b>	Zip Code: <b>19966</b>	
3.	Site Name: Millsboro Complex			
4.	Site Mailing Address: (if different from above)			
	City:	State:	Zip Code:	
5.	Physical Location of Site: <b>29106 John J.</b> (if different from above)	Williams Hwy		
	City: Millsboro	State: Delaware	Zip Code: <b>19966</b>	
6.	Site Billing Address: (if different from above)			
	City:	State:	Zip Code:	
<b>7.</b> .	Air Quality Management Facility ID Number	er: 1000500004		
8.	Site NAICS Code): <b>31165, 311119, 11234</b> (list all that apply			
9.	Site SIC Code: <b>2015</b> , <b>2048</b> , <b>0254</b> (list all that apply)			
10.	Site Location Coordinates: Latitude: Longitude	38 ° 36' 2.3508" : 75 ° 15' 24.2288"		
11.	Is the Facility New or Existing?	☐ NEW ☐ EXISTING		
If the	Facility is an Existing Facility, Complete the	e Rest of Question 11. If No	ot, Proceed to Question 12.	
11.1.	Does the Facility Have Active Air Permits'	? ⊠YES	□NO	
12.	Is this Application For New Equipment or ☐ New Equipment ☐ Modification of Existing Equipment ☐ Other (Specify):	•		
	application is for the modification of existinged to Question 13	g equipment, complete the	rest of Question 12. If not,	



Form AQM-1 Page 2 of 4

Company and Site Information			
12.1. Does the Equipment Have an Active Air Permit? XYES NO			
If the equipment has an active air permit, complete the rest of Question 12. If not, proceed to Question 13.			
12.2. Permit Number of Existing Equipment: APC-2014/0090-OPERATION (Amendment 1)			
13. Status of Equipment Being Applied For:  ☐ Synthetic Minor Source ☐ Major Source ☐ Hederally Enforceable Restrictions			
14. Facility Status: 🛛 Natural Minor Facility 🔲 Synthetic Minor Facility 🔲 Major Facility			
If the facility is a Major Source, complete the rest of Question 14. If not, proceed to Question 15.			
14.1. Responsible Official Name: Jimmy Paulakuhn			
14.2. Responsible Official Title: VP of Live Operations			
Contact Information			
15. Name of Owner or Facility Manager: Jimmy Paulakuhn			
16. Title of Owner or Facility Manager: VP of Live Operations			
17. Permit Contact Name: Austin Pajda			
18. Permit Contact Title: Environmental Manager			
19. Permit Contact Telephone Number: 302-934-3070			
20. Permit Contact Fax Number:			
21. Permit Contact E-Mail Address: apajda@mountaire.com			
22. Billing Contact Name:			
23. Billing Contact Title:			
24. Billing Contact Telephone Number:			
25. Billing Contact Fax Number:			
26. Billing Contact E-Mail Address:			
Proposed Construction and Operating Schedule			
27. When Will the Proposed Construction/Installation/Modification Occur: upon amendment approval			
28. Proposed Operating Schedule: <b>24</b> hours/day <b>7</b> days/week <b>52</b> weeks/year			
28.1. Is There Any Additional Information Regarding the Operating Schedule? YES NO			
If YES, complete the rest of Question 28. If NO, proceed to Question 29.			



Form AQM-1 Page 3 of 4

#### **Proposed Construction and Operating Schedule**

28.2. Describe the Additional Information: The pellet cooler is being replaced. All associated air equipment is remaining.

equipment is remaining.
Coastal Zone Information
29. Is the Facility Located in the Coastal Zone? X YES NO
If the facility is located in the Coastal Zone complete the rest of Question 29. If not, proceed to Question 30.
29.1. Is a Coastal Zone Permit Required for Construction or Operation of the Source Being Applied for? ☐ YES ☐ NO
Attach a copy of the Coastal Zone Determination if it has not been previously submitted
If a Coastal Zone Permit is required complete the rest of Question 29. If not, proceed to Question 30.
29.2. Has a Coastal Zone Permit Been Issued?
Attach a copy of the Coastal Zone Permit if it has not been previously submitted
Local Zoning Information
30. Parcel Zoning: H-1; Heavy Industrial
Attach Proof of Local Zoning if it has not been previously submitted
Application Information
31. Is the Appropriate Application Fee Attached? ☐ YES ☐ NO
32. Is the Advertising Fee Attached? ⊠ YES □ NO
For help determining your application and advertising fees see:
http://www.dnrec.state.de.us/DNREC2000/Library/Fees/DE%20Permit%20Fees.htm  Attach the appropriate fees. Note that your Application will not be considered complete if the appropriate fees are not included.
33. Is a Cover Letter Describing the Process Attached? ☐ YES ☐ NO
Attach a brief cover letter describing your Application.
If the Facility is a New Facility complete Question 34. If not, proceed to Question35.
34. Is a Copy of the Applicant Background Information Questionnaire on Record at the Department? ☐ YES ☐ NO
If NO, complete the rest of Question 34. If YES, process to Question 35.
34.1 Is a Copy of the Applicant Background Information Questionnaire Attached?
For a copy of the Applicant Background Information Questionnaire see <a href="http://www.dnrec.delaware.gov/services/Documents/Chapter79Form.pdf">http://www.dnrec.delaware.gov/services/Documents/Chapter79Form.pdf</a>
Attach a copy of the Applicant Background Information Questionnaire if applicable.
35. Check Which Application Forms are Attached:



Form AQM-1 Page 4 of 4

Application Information						
AQM-1       AQM-3.4       AQM-3.9       AQM-3.14       AQM-4.4       AQM-4.9       AQM-6         AQM-2       AQM-3.5       AQM-3.10       AQM-3.15       AQM-4.5       AQM-4.10         AQM-3.1       AQM-3.6       AQM-3.11       AQM-4.1       AQM-4.6       AQM-4.11         AQM-3.2       AQM-3.7       AQM-3.12       AQM-4.2       AQM-4.7       AQM-4.12         AQM-3.3       AQM-3.8       AQM-3.13       AQM-4.3       AQM-4.8       AQM-5						
36. Check Which Documents are Attached:  Coastal Zone Determination  Manufacturer Specification(s)						
☐ Coastal Zone Permit       ☐ Material Safety Data Sheets (MSDSs)         ☐ Proof of Local Zoning       ☐ Material Safety Data Sheets (MSDSs)         ☐ Application Fee       ☐ Descriptive Cover Letter         ☐ Other (Specify):						
Confidentiality Information						
37. Do You Consider Any of the Information Submitted With this Application Confidential?  For help on how to submit a confidentiality claim see <a href="http://regulations.delaware.gov/register/december2011/final/15%20DE%20Reg%20864%2012-01-11.htm">http://regulations.delaware.gov/register/december2011/final/15%20DE%20Reg%20864%2012-01-11.htm</a> If a Claim of Confidentiality is made it MUST meet the requirements of Section 6 of DNREC's Freedom of Information ("FOIA") Regulation at the time the Application is submitted.						
Signature Block						
I, the undersigned, hereby certify under penalty of law that I have personally examined and am familiar with the information submitted in this document and all of its attachments as to the truth, accuracy, and completeness of this information. I certify based on information and belief formed after reasonable inquiry, the statements and information in this document are true, accurate, and complete. By signing this form, I certify that I have not changed, altered, or deleted any portions of this application. I acknowledge that I cannot commence construction, alteration, modification or initiate operation until I receive written approval (i.e. permit, registration, or exemption letter) from the Department. I acknowledge that I may be required to perform testing of the equipment to receive construction or operation approval, and that if I do not receive approval to construct or operate that I may appeal the decision.  Jimmy Paulakuhn  Owner or Operator  Signature of Owner or Operator						

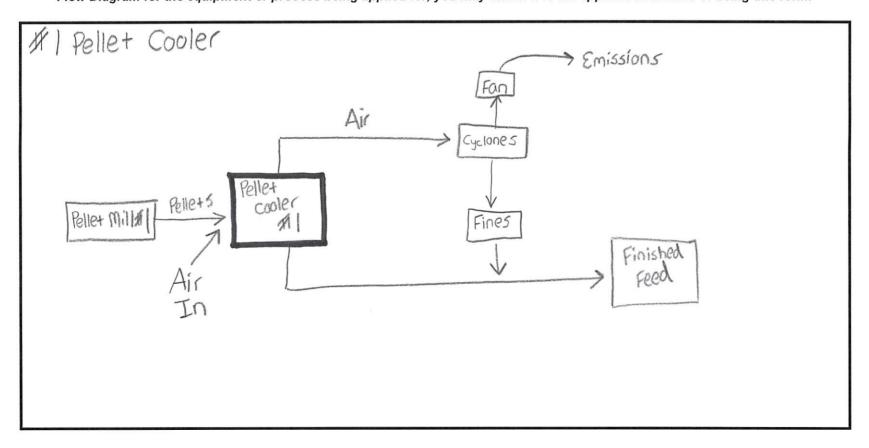
One Original and One Copy of All Application Forms Should Be Mailed To: Division of Air Quality 100 W. Water Street, Suite 6A Dover, Delaware 19904

> All Checks Should Be Made Payable To: State of Delaware

Form AQM-2 Page 1 of 1

#### **Process Flow Diagram**

Sketch the Process Flow Diagram for the equipment or process being applied for. Include each emission unit and control device (even existing emission units that will not be modified by this application). You may identify each emission unit with a simple shape. Label each emission unit and control device with a unique identifier. Show the relationship between each emission unit and/or control device by drawing arrows between them to indicate the flow of air pollutants. List which application forms are included for each emission unit or control device below the shape representing each emission unit or control device. See <a href="http://www.delaware.gov/reg2/default.htm">http://www.delaware.gov/reg2/default.htm</a> for example Process Flow Diagrams for common processes. If you already have a Process Flow Diagram for the equipment or process being applied for, you may attach it to the application instead of using this form.



Form AQM-3.13 Page 1 of 11

## Grain Terminal, Elevator, and Drying Application

If you are using this form electronically, press F1 at any time for help

	General Information						
1.	Facility Name: Millsboro Feed Mill						
2.	2. Types of Grain Handling Activities: (check all that apply)  Receiving: Truck Unloading Receiving: Railcar Unloading Receiving: Barge Unloading Transferring and Conveying: Receiving Elevator Leg Transferring and Conveying: Elevator Head (Headhouse) Transferring and Conveying: Storage Bin Vents Transferring and Conveying: Turning Grain Processing: Scales (Microunits) Grain Processing: Hammermills Grain Processing: Mixers Grain Processing: Pellet Coolers Screening and Cleaning Grain Drying Shipping (Load Out): Truck Loading Shipping (Load Out): Railcar Loading Shipping (Load Out): Barge Loading Other (Specify):						
3.	Year Facility Installed:	1983					
4.	Permanent Grain Stor	age Capacity: 6.2	million bushels				
		Grain Re	eceiving Information	<u>on</u>			
If Gra	ain Receiving activities o	lo not occur, procee	ed to Question 9.				
5.	Types of Vehicles Unl	oaded and Grain R	eceived (check all that	apply)			
If there		If there are more than five combinations of Vehicles Unloaded and Grain Received, attach additional copies of this page as					
						buge ne	
	Type of Vehicle Unloaded	Type of Grain Unloaded	Method of Unloading	Grain Density (lb/bushel)	Maximum Quantity Unloaded (tons/hour)	Maximum Quantity Unloaded (tons/year)	
5.1.				Density	Maximum Quantity Unloaded	Maximum Quantity Unloaded	



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	Grain Receiving Information					
	Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	☐ Gravity Dump ☐ Other (Specify):			
5.3.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):			
5.4.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	☐ Corn ☐ Wheat ☐ Rye ☐ Oats ☐ Barley ☐ Flax Seed ☐ Sorghum ☐ Soybeans ☐ Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):			
5.5.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):			
6.	Number of Receiving	Areas at this Facility	y:			
7.	Maximum Hourly Grain		Receiving Areas:	bushels		
8.	8. Describe Grain Receiving Equipment:					
	G-	ain Transforrin	a and Convoving	Information	•	
If Gra	ain Transferring and Cor		g and Conveying		<u>.</u>	



Form AQM-3.13 Page 3 of 11

	Grain Transferring and Conveying Information						
9.	9. Grain Transferring and Conveying Information						
If there	If there are more than five types of grain transferred or conveyed, attach additional copies of this page as needed.						
	Type of Grain	Maximum Quantity Transfe Conveyed (tons/hour)		Quantity Transferred d (tons/year)			
9.1.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rye ☐ Soybeans ☐ Dats ☐ Barley ☐ Other (Specify):						
9.2.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rye ☐ Soybeans ☐ Dats ☐ Barley ☐ Other (Specify):						
9.3.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rye ☐ Soybeans ☐ Dats ☐ Barley ☐ Other (Specify):						
9.4.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rye ☐ Soybeans ☐ Dats ☐ Barley ☐ Other (Specify):						
9.5	□ Corn □ Flax Seed   □ Wheat □ Sorghum   □ Rye □ Soybeans   □ Oats □ Barley   □ Other (Specify):						
10.	Describe Grain Transferring and 0	Conveying Equipment:					
	Gra	ain Processing Informa	ation_				
If Gra	in Processing activities do not occi	ur, proceed to Question 13.					
11.	Grain Processing Information						
If there	e are more than five combinations of gra						
	Type of Grain	Processing Operation	Maximum Quantity Processed (tons/hour)	Maximum Quantity Processed (tons/year)			
11.1.	□ Corn     □ Flax Seed     □ Wheat     □ Sorghum     □ Rye     □ Soybeans     □ Oats     □ Barley     □ Other (Specify):	Scales Hammermills	50	438000			



Form AQM-3.13 Page 4 of 11

Grain Processing Information							
11.2.	Corn Flax Seed Wheat Sorghum Rye Soybeans Oats Barley Other (Specify):	☐ Scales ☐ Hammermills ☐ Mixers ☐ Pellet Coolers ☐ Other (Specify):					
11.3.	Corn Flax Seed Wheat Sorghum Rye Soybeans Oats Barley Other (Specify):	☐ Scales ☐ Hammermills ☐ Mixers ☐ Pellet Coolers ☐ Other (Specify):					
11.4.	Corn Flax Seed Wheat Sorghum Rye Soybeans Oats Barley Other (Specify):	☐ Scales ☐ Hammermills ☐ Mixers ☐ Pellet Coolers ☐ Other (Specify):					
11.5	Corn Flax Seed Wheat Sorghum Rye Soybeans Oats Barley Other (Specify):	☐ Scales ☐ Hammermills ☐ Mixers ☐ Pellet Coolers ☐ Other (Specify):					
12.	12. Is Any Other Material Added to the Grain During Processing? ☐ YES ☒ NO						
If YES	S, complete the rest of Question	12. If NO, proceed to Question 13.					
12.1.	Describe the Material(s) Added	and the Mixing Ratio:					
	Grain C	eaning and Screening Informa	<u>ation</u>				
If Gra	in Cleaning and Screening activi	ties do not occur, proceed to Question	15.				
13.	Grain Cleaning and Screening	nformation					
If there	e are more than five types of grain clea	ned and/or screened, attach additional copie	es of this page as needed.				
	Type of Grain	Maximum Quantity Cleaned or Screened (tons/hour)	Maximum Quantity Cleaned or Screened (tons/year)				
13.1.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rye ☐ Soybeans ☐ Dats ☐ Barley ☐ Other (Specify):						
13.2.	☐ Corn ☐ Flax Seed ☐ Wheat ☐ Sorghum ☐ Rive ☐ Soryheans						



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Grain Cleaning and Screening Information				
	☐ Oats ☐ Barley ☐ Other (Specify):			
13.3.	Corn Flax Seed Wheat Sorghum Rye Soybeans Oats Barley Other (Specify):			
13.4.	□ Corn □ Flax Seed   □ Wheat □ Sorghum   □ Rye □ Soybeans   □ Oats □ Barley   □ Other (Specify):			
13.5	□ Corn □ Flax Seed   □ Wheat □ Sorghum   □ Rye □ Soybeans   □ Oats □ Barley   □ Other (Specify):			
14.	Describe Grain Cleaning and Screening Equipment:			
	Grain Drying Information			
If Gra	n Drying activities do not occur, proceed to Question 33.			
15.	Grain Dryer Equipment ID Number:			
16.	Grain Dryer Type: ☐ Column Dryer ☐ Rack Dryer ☐ Other (Specify):			
17.	Manufacturer:			
18.	Model:			
19.	Serial Number:			
20.	Maximum Design Grain Input Capacity at 5 Points Moisture Removal: bushels/hour			
21.	Design Operating Temperature: °F			
22.	Number of Burners in Dryer:			
23.	Rated Heat Input of Burners: MMBTU/hr			
24.	Total Rated Heat Input of Dryer: MMBTU/hr			
25.	Fuel Used:  Natural Gas Diesel No. 2 Fuel Oil No. 4 Fuel Oil No. 6 Fuel Oil Other (specify):			
25.1.	Maximum Annual Fuel Consumption: MMCF			
25.2.	Heat Content of Fuel: BTU/MMCF			



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Grain Drying Information							
25.3.	Maximum Firing Ra	te: MMCF	/hr				
25.4.	Percent Sulfur of Fu	ıel: %					
26.	Airflow Through Dry	er: cubic	feet/mi	nute			
27.	Grain Dried						
	Grain	Grain Density (Ib/bushel)		mum Hourly Input /hour)		kimum Annual s/year)	Throughput
27.1.	Corn						
27.2.	Wheat						
27.3.	Rye						
27.4.	Oats						
27.5	Barley						
27.6.	Flax Seed						
27.7.	Sorghum						
27.8.	Soybeans						
27.9.							
28.	Average Design Per	rcent Moisture In	Grain A	After Drying:	%		
29.	Grain Dryer Diamete	er: <b>feet</b>			F		
30.	Grain Dryer Height:	feet					
31.	Height of Grain Drye	er Exhaust Sectio	n:	feet			
32.	U.S. Sieve or Tyler	Scale Mesh Scree	en Size	: Tyler Sca	le Mesh Size	9	
		Grain Ship	ping	(Load Out) Info	rmation		
If Gra	in Shipping activities	do not occur, pro	ceed to	Question 37.			
33.	Types of Vehicles L	oaded and Grain	Shippe	ed (check all that app	oly)		
If there	are more than five com	binations of Vehicles	Loade	d and Grain Shipped, at	tach additiona		
	Type of Vehicle Loaded	Type of Gr Shipped	<u>ain</u>	Method of Loading	Grain Density (lb/bushel)	Maximum Quantity Loaded (tons/hour)	Maximum Quantity Loaded (tons/year)
33.1.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Ca Continuous Bary Marine Leg Ship Other (Specify):	ge Barley Flax Se	m	Conveyor Pneumatic Gravity Dump Other (Specify):			



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	<u>(</u>	Grain Shipping	(Load Out) Info	rmation	
		Other (Specify):			
33.2.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):		
33.3.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):		
33.4.	Straight Truck Hopper Truck Rail: Boxcar Rail: Hopper Car Continuous Barge Marine Leg Ship Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):		
33.5.	☐ Straight Truck ☐ Hopper Truck ☐ Rail: Boxcar ☐ Rail: Hopper Car ☐ Continuous Barge ☐ Marine Leg ☐ Ship ☐ Other (Specify):	Corn Wheat Rye Oats Barley Flax Seed Sorghum Soybeans Other (Specify):	Conveyor Pneumatic Gravity Dump Other (Specify):		
34.	Number of Loading Area		,		
35.	Maximum Hourly Grain T		oading Areas:	bushels	
36.	Describe Grain Loading	Equipment:			



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Control Device Information					
37. Is an Air Pollution Control Device Used?  ☐ YES ☐ NO					
If an Air Pollution Control Device is used, complete the rest of Question 37. If not, proceed to Question 38.					
37.1. Is Knockout Used? ☐ YES ☒ NO					
If YES, complete Form AQM-4.11 and attach it to this application.					
37.2. Is a Settling Chamber Used? ☐ YES ☒ NO					
If YES, complete Form AQM-4.10 and attach it to this application.					
37.3. Is an Inertial or Cyclone Collector Used?   ☐ YES ☐ NO					
If YES, complete Form AQM-4.5 and attach it to this application.					
37.4. Is a Fabric Collector or Baghouse Used? ☐ YES ☒ NO					
If YES, complete Form AQM-4.6 and attach it to this application.					
37.5. Is a Venturi Scrubber Used? ☐ YES ☐ NO					
If YES, complete Form AQM-4.8 and attach it to this application.					
37.6. Is an Electrostatic Precipitator Used? ☐ YES ☐ NO					
If YES, complete Form AQM-4.7 and attach it to this application.					
37.7. Is Any Other Control Device Used? ☐ YES ☐ NO					
If YES, attach a copy of the control device Manufacturer's Specification Sheet(s).					
If any other control device is used, complete the rest of Question 37. If not, proceed to Question 38.					
37.8. Describe Control Device:					
37.9. Pollutants Controlled: PM PM <sub>10</sub> PM <sub>2.5</sub> Other (Specify):					
37.10. Control Device Manufacturer:					
37.11. Control Device Model:					
37.12. Control Device Serial Number:					
37.13. Control Device Design Capacity:					
37.14. Control Device Removal or Destruction Efficiency:					
Stack Information					
38. How Does the Process Equipment Vent: (check all that apply) ☐ Directly to the Atmosphere ☐ Through a Control Device Covered by Forms AQM-4.1 through 4.12 ☐ Through Another Control Device Described on This Form					
If any of the process equipment vents directly to the atmosphere or through another control device described on this form, proceed to Question 39. If the process equipment vents through a control device, provide the stack parameters on the control device form and proceed to Question 43.					
39. Number of Air Contaminant Emission Points:					
If there are more than three Emission Points, attach additional copies of this page as needed.					
For the first Emission Point					



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Stack Information			
40. Emission Point Name:			
40.1. Stack Height Above Grade: feet			
40.2. Stack Exit Diameter: <b>feet</b> (Provide Stack Dimensions If Rectangular Stack)			
40.3. Is a Stack Cap Present?			
40.4. Stack Configuration:			
40.5. Stack Exit Gas Temperature: °F			
40.6. Stack Exit Gas Flow Rate: ACFM			
40.7. Distance to Nearest Property Line: feet			
40.8. Describe Nearest Obstruction:			
40.9. Height of Nearest Obstruction: feet			
40.10. Distance to Nearest Obstruction: feet			
40.11. Are Stack Sampling Ports Provided?			
For the second Emission Point. If there is no second Emission Point, proceed to Question 43.			
41. Emission Point Name:			
41.1. Stack Height Above Grade: feet			
41.2. Stack Exit Diameter: feet (Provide Stack Dimensions If Rectangular Stack)			
41.3. Is a Stack Cap Present?			
41.4. Stack Configuration: Vertical Horizontal Downward-Venting (check all that apply) Other (Specify):			
41.5. Stack Exit Gas Temperature: °F			
41.6. Stack Exit Gas Flow Rate: ACFM			
41.7. Distance to Nearest Property Line: feet			
41.8. Describe Nearest Obstruction:			
41.9. Height of Nearest Obstruction: feet			
41.10. Distance to Nearest Obstruction: feet			
41.11. Are Stack Sampling Ports Provided?			
For the third Emission Point. If there is no third Emission Point, proceed to Question 43.			
42. Emission Point Name:			
42.1. Stack Height Above Grade: feet			
42.2. Stack Exit Diameter: <b>feet</b> (Provide Stack Dimensions If Rectangular Stack)			
42.3. Is a Stack Cap Present?			
42.4. Stack Configuration:  Vertical  Horizontal Downward-Venting (check all that apply) Other (Specify):			
42.5. Stack Exit Gas Temperature: °F			



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	Stack Information					
42.6.	Stack Exit Gas Flow Ra	ate: ACFM				
42.7.	Distance to Nearest Pro	operty Line: fe	eet			
42.8. [	Describe Nearest Obst	ruction:				
42.9. H	Height of Nearest Obst	ruction: feet				
42.10.	42.10. Distance to Nearest Obstruction: feet					
42.11. A	Are Stack Sampling Po	rts Provided?	☐ YES ☐ NO			
	Visible Emissions Monitoring Information					
43. F	Proposed Technique U	sed to Monitor Visible	☐ Manual (N	Monitor (COM) Method 9) Method 22) escribe):		
If an Op	If an Opacity Monitor (COM) is used, complete the rest of Question 43. If not, proceed to Question 44.					
43.1. [	Describe the Continuou	us Opacity Monitoring	g System:			
43.2. I	Manufacturer:					
43.3. N	Model:					
43.4.	Serial Number:					
44. F	Proposed Frequency o	f Opacity Monitoring:				
		Monitoring ar	nd Alarm Information			
	Are There Any Alarms When Drafting the Perr		Department to Consider	☐ YES ⊠ NO		
If YES,	complete the rest of Q	uestion 45. If NO, pr	oceed to Question 46.			
	Describe the System A					
If there a	re more than five alarms, a Operating			5 11 11 1 12 1		
	Parameter Monitored	Describe Alarm Trigger	Monitoring Device or Alarm Type	Does the Alarm Initiate an Automated Response?		
45.1.1.			☐ Visual ☐ Auditory ☐ Automatic (Remote Monitoring) ☐ Other	NO YES Describe:		
45.1.2.			☐ Visual ☐ Auditory ☐ Automatic (Remote Monitoring) ☐ Other	□ NO □ YES Describe:		
45.1.3.			☐ Visual	□ NO □ YES		



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Monitoring and Alarm Information								
	☐ Auditory Describe: ☐ Automatic (Remote Monitoring) ☐ Other ☐ Visual ☐ NO ☐ VES							
45.1.4.	Auditory Automatic (Remote Monitoring) Other							
45.1.5.	☐ Visual ☐ NO ☐ YES ☐ Auditory ☐ Describe: ☐ (Remote Monitoring) ☐ Other							
Volunt	Voluntary Emission Limitation Request Information							
46. Are You Requesting Any Voluntary Emission Limitations to Avoid Major Source Status, Minor New Source Review, MACT, NSPS, etc.?  If YES, complete the rest of Question 46. If NO, proceed to Question 47.  46.1. Describe Any Proposed Emission Limitations:								
Volunt	ary Operating Limitation Request Information							
	/ Voluntary Operating Limitations to Avoid nor New Source Review, MACT, NSPS, etc.? ☐ YES ☐ NO							
	uestion 47. If NO, proceed to Question 48.							
47.1. Describe Any Proposed	Operating Limitations:							
Additional Information								
48. Is There Any Additional	Information Pertinent to this Application?   ☐ YES ☐ NO							
If YES, complete the rest of Qu	New York (1997) (1997) (1997)							
from the previous pell	ice information per AQM 4.1 is not changing and should be referenced et cooler #1 permit application (Koger-Air model 2H54 high efficiency odification is the replacement of the pellet cooler itself.	d						

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## **Emissions Information Application**

If you are using this form electronically, press F1 at any time for help

#### **Process Information**

- 1. Number of Individual Pieces of Process Equipment in Process: 1
- 2. Number of Individual Control Devices in Process: 1

#### **Emissions Information for First Emission Point/Stack**

- 3. Emission Point Name: #1 Pellet Cooler
- 4. Equipment ID Number for all Process Equipment and Control Devices Venting Through Emission Point/Stack: #1 Pellet Cooler
- 5. Pollutant Emissions

If more than 15 pollutants are emitted at this Emission Point/Stack, attach additional copies of this page as needed.

	Pollutant Name (Specify VOCs and HAPs Individually in 5.10 through 5.18)	CAS Number (Not required for 5.1 through 5.10)	Maximum Uncontrolled Emission Rate at Design Capacity	Maximum Controlled Emission Rate at Design Capacity	Annual Potential to Emit (PTE)	Requested Permitted Annual Emissions
5.1.	Particulate Matter (PM)		lbs/hour	lbs/hour	tons/year	tons/year
5.2.	PM <sub>10</sub>	N/A	3.75 lbs/hour	3.75 lbs/hour	16.425 tons/year	16.425 tons/year
5.3.	PM <sub>2.5</sub>		lbs/hour	lbs/hour	tons/year	tons/year
5.4.	Sulfur Oxides (SO <sub>X</sub> )		lbs/hour	lbs/hour	tons/year	tons/year
5.5.	Nitrogen Oxides (NOx)		lbs/hour	lbs/hour	tons/year	tons/year
5.6.	Carbon Monoxide (CO)		lbs/hour	lbs/hour	tons/year	tons/year
5.7.	Total Volatile Organic Compounds (VOCs)		lbs/hour	lbs/hour	tons/year	tons/year
5.8.	Total Hazardous Air		lbs/hour	lbs/hour	tons/year	tons/year

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Pollutants (HAPs)				
5.9. CO <sub>2</sub>	lbs/hour	lbs/hour	tons/year	tons/year
5.10. CO <sub>2e</sub>	lbs/hour	lbs/hour	tons/year	tons/year
5.11.	lbs/hour	lbs/hour	tons/year	tons/year
5.12.	lbs/hour	lbs/hour	tons/year	tons/year
5.13.	lbs/hour	lbs/hour	tons/year	tons/year
5.14.	lbs/hour	lbs/hour	tons/year	tons/year
5.15.	lbs/hour	lbs/hour	tons/year	tons/year
6. Provide Any Additional Infor	nation Necessary to Understanding the Emiss	ion Rates Provided Above:	•	

	Emissions Information for Second Emission Point/Stack					
7.	Emission Point Name:					
8.	Equipment ID Number for all Process Equipment and Control Devices Venting Through Emission Point/Stack:					
9.	Pollutant Emissions					
If mo	re than 15 pollutants are emitted at th	is Emission Point/Sta	ack, attach additional copies of	this page as needed.		
	Pollutant Name (Specify VOCs and HAPs Individually in 9.10 through 9.18)	CAS Number (Not required for 9.1 through 9.10)	Maximum Uncontrolled Emission Rate at Design Capacity	Maximum Controlled Emission Rate at Design Capacity	Annual Potential to Emit (PTE)	Requested Permitted Annual Emissions
9.1.	Particulate Matter (PM)		lbs/hour	lbs/hour	tons/year	tons/year
9.2.	PM <sub>10</sub>		lbs/hour	lbs/hour	tons/year	tons/year

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9.3.	PM <sub>2.5</sub>	lbs/hour	lbs/hour	tons/year	tons/yea
9.4.	Sulfur Oxides (SO <sub>x</sub> )	lbs/hour	lbs/hour	tons/year	tons/yea
9.5.	Nitrogen Oxides (NOx)	lbs/hour	lbs/hour	tons/year	tons/yea
9.6.	Carbon Monoxide (CO)	lbs/hour	lbs/hour	tons/year	tons/yea
9.7.	Total Volatile Organic Compounds (VOCs)	lbs/hour	lbs/hour	tons/year	tons/yea
9.8.	Total Hazardous Air Pollutants (HAPs)	lbs/hour	lbs/hour	tons/year	tons/yea
9.9.	CO <sub>2</sub>	lbs/hour	lbs/hour	tons/year	tons/yea
9.10.	CO <sub>2e</sub>	lbs/hour	lbs/hour	tons/year	tons/yea
9.11.		lbs/hour	lbs/hour	tons/year	tons/yea
9.12.		lbs/hour	lbs/hour	tons/year	tons/yea
9.13.		lbs/hour	lbs/hour	tons/year	tons/yea
9.14.		lbs/hour	lbs/hour	tons/year	tons/yea
9.15.		lbs/hour	lbs/hour	tons/year	tons/ye

Attach the Basis of Determination or Calculations for each Emission Rate provided above.

## **Emissions Information for Third Emission Point/Stack**

- 11. Emission Point Name:
- 12. Equipment ID Number for all Process Equipment and Control Devices Venting Through Emission Point/Stack:
- 13. Pollutant Emissions

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	Emissions Information for Third Emission Point/Stack					
If more t	han 15 pollutants are emitted at t	his Emission Point/Sta	ck, attach additional copies of	this page as needed.		
	Pollutant Name (Specify VOCs and HAPs Individually in 13.10 through 13.18)	CAS Number (Not required for 13.1 through 13.10)	Maximum Uncontrolled Emission Rate at Design Capacity	Maximum Controlled Emission Rate at Design Capacity	Annual Potential to Emit (PTE)	Requested Permitted Annual Emissions
13.1.	Particulate Matter (PM)		lbs/hour	lbs/hour	tons/year	tons/year
13.2.	PM <sub>10</sub>		lbs/hour	lbs/hour	tons/year	tons/year
13.3.	PM <sub>2.5</sub>		lbs/hour	lbs/hour	tons/year	tons/year
13.4.	Sulfur Oxides (SOx)		lbs/hour	lbs/hour	tons/year	tons/year
13.5.	Nitrogen Oxides (NOx)		lbs/hour	lbs/hour	tons/year	tons/year
13.6.	Carbon Monoxide (CO)		lbs/hour	lbs/hour	tons/year	tons/year
13.7.	Total Volatile Organic Compounds (VOCs)		lbs/hour	lbs/hour	tons/year	tons/year
13.8.	Total Hazardous Air Pollutants (HAPs)		lbs/hour	lbs/hour	tons/year	tons/year
13.9.	CO <sub>2</sub>		lbs/hour	lbs/hour	tons/year	tons/year
13.10.	CO <sub>2e</sub>		lbs/hour	lbs/hour	tons/year	tons/year
13.11.			lbs/hour	lbs/hour	tons/year	tons/year
13.12.			lbs/hour	lbs/hour	tons/year	tons/year
13.13.			lbs/hour	lbs/hour	tons/year	tons/year
13.14.			lbs/hour	lbs/hour	tons/year	tons/year
13.15.			lbs/hour	lbs/hour	tons/year	tons/year
14. F	Provide Any Additional Inforn	nation Necessary to	Understanding the Emiss	ion Rates Provided Above	o:	

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#### **Emissions Information for Third Emission Point/Stack**

Attach the Basis of Determination or Calculations for each Emission Rate provided above.

#### **Emissions Information for Fourth Emission Point/Stack**

- 15. Emission Point Name:
- 16. Equipment ID Number for all Process Equipment and Control Devices Venting Through Emission Point/Stack:
- 17. Pollutant Emissions

If more than 15 pollutants are emitted at this Emission Point/Stack, attach additional copies of this page as needed.

	Pollutant Name (Specify VOCs and HAPs Individually in 17.10 through 17.18)	CAS Number (Not required for 17.1 through 17.10)	Maximum Uncontrolled Emission Rate at Design Capacity	Maximum Controlled Emission Rate at Design Capacity	Annual Potential to Emit (PTE)	Requested Permitted Annual Emissions
17.1.	Particulate Matter (PM)		lbs/hour	lbs/hour	tons/year	tons/year
17.2.	PM <sub>10</sub>		lbs/hour	lbs/hour	tons/year	tons/year
17.3.	PM <sub>2.5</sub>		lbs/hour	lbs/hour	tons/year	tons/year
17.4.	Sulfur Oxides (SOx)		lbs/hour	lbs/hour	tons/year	tons/year
17.5.	Nitrogen Oxides (NOx)		lbs/hour	lbs/hour	tons/year	tons/year
17.6.	Carbon Monoxide (CO)		lbs/hour	lbs/hour	tons/year	tons/year
17.7.	Volatile Organic Compounds (VOCs)		lbs/hour	lbs/hour	tons/year	tons/year
17.8.	Total Hazardous Air Pollutants (HAPs)		lbs/hour	lbs/hour	tons/year	tons/year
17.9.	CO <sub>2</sub>		lbs/hour	lbs/hour	tons/year	tons/year
17.10.	CO <sub>2e</sub>		lbs/hour	lbs/hour	tons/year	tons/year
17.11.		e e	lbs/hour	lbs/hour	tons/year	tons/year
17.12.			lbs/hour	lbs/hour	tons/year	tons/year

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Emissions Information for Fourth Emission Point/Stack						
lbs/hour	lbs/hour	tons/year	tons/year			
lbs/hour	lbs/hour	tons/year	tons/year			
lbs/hour	lbs/hour	tons/year	tons/year			
	lbs/hour lbs/hour	lbs/hour lbs/hour lbs/hour	Ibs/hour   Ibs/hour   tons/year			

18. Provide Any Additional Information Necessary to Understanding the Emission Rates Provided Above:

Attach the Basis of Determination or Calculations for each Emission Rate provided above.

If there are more than four Emission Points/Stacks, attach additional copies of this form as needed.

#### **Overall Process Emissions**

#### 19. Pollutant Emissions

If more than 15 pollutants are emitted from this Process, attach additional copies of this page as needed.

	Pollutant Name (Specify VOCs and HAPs Individually in 19.10 through 19.18)	CAS Number (Not required for 19.1 through 19.10)	Maximum Uncontrolled Emission Rate at Design Capacity	Maximum Controlled Emission Rate at Design Capacity	Annual Potential to Emit (PTE)	Requested Permitted Annual Emissions
19.1.	Particulate Matter (PM)		lbs/hour	lbs/hour	tons/year	tons/year
19.2.	PM <sub>10</sub>		3.75 lbs/hour	3.75 lbs/hour	<b>16.425</b> tons/year	16.425 tons/year
19.3.	PM <sub>2.5</sub>		lbs/hour	lbs/hour	tons/year	tons/year
19.4.	Sulfur Oxides (SO <sub>X</sub> )		lbs/hour	lbs/hour	tons/year	tons/year
19.5.	Nitrogen Oxides (NOx)		lbs/hour	lbs/hour	tons/year	tons/year
19.6.	Carbon Monoxide (CO)		lbs/hour	lbs/hour	tons/year	tons/year
19.7.	Total Volatile Organic Compounds (VOCs)		lbs/hour	lbs/hour	tons/year	tons/year
19.8.	Total Hazardous Air Pollutants (HAPs)		lbs/hour	lbs/hour	tons/year	tons/year

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lbs/hour lbs/hour	lbs/hour	tons/year	tons/year				
lbs/hour	lbs/bour						
	ibanioui	tons/year	tons/year				
lbs/hour	lbs/hour	tons/year	tons/year				
lbs/hour	lbs/hour	tons/year	tons/year				
lbs/hour	lbs/hour	tons/year	tons/year				
lbs/hour	lbs/hour	tons/year	tons/year				
20. Provide Any Additional Information Necessary to Understanding the Emission Rates Provided Above:  Attach the Basis of Determination or Calculations for each Emission Rate provided above.							
	Ibs/hour Ibs/hour Ibs/hour Understanding the Emissi	Ibs/hour Ibs/hour Ibs/hour Ibs/hour Ibs/hour Ibs/hour Ibs/hour Understanding the Emission Rates Provided Above:	Ibs/hour   Ibs/hour   tons/year     Ibs/hour   Ibs/hour   tons/year     Ibs/hour   Ibs/hour   tons/year     Understanding the Emission Rates Provided Above:				

		Minor New Source Review Information	
21.	Does the Process Have the Pote	ntial to Emit More Than Five Tons Per Year of Any Pollutant?	☑ YES ☐ NO
22.	Is the Source New or Existing? See Question 11 of AQM-1	□ NEW ⊠ EXISTING	
	Process has the Potential to Emit more to Section 4 must be conducted and attach	than five tons per year of any pollutant, and is a New Source, a Control Te ed to this application.	chnology Analysis pursuant to Regulation No.

## **Major New Source Review Information**

23. Does the Process Have the Potential to Emit More Than the Significance Level for Any Pollutant? (Check All That Apply)



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If th (302	☐ Greater Than 25 Tons Per Year of Particulate Matter (PM) ☐ Greater Than 15 Tons Per Year of PM₁0 ☐ Greater Than 10 Tons Per Year of PM₂.5 ☐ Greater Than 40 Tons Per Year of Sulfur Dioxide(SO₂) ☐ Greater Than 25 Tons Per Year of Nitrogen Oxides (NOҳ) in New Castle and Kent County ☐ Greater Than 100 Tons Per Year of Nitrogen Oxides (NOҳ) in Sussex County ☐ Greater Than 100 Tons Per Year of Carbon Monoxide (CO) ☐ Greater Than 25 Tons Per Year of Total Volatile Organic Compounds (VOCs) in New Castle and Kent County ☐ Greater Than 50 Tons Per Year of Total Volatile Organic Compounds (VOCs) in Sussex County ☐ Greater Than 75,000 Tons Per Year of Equivalent Carbon Dioxide (CO₂e)  The Process has the Potential to Emit greater than any of the amounts listed above 7 DE Admin. Code 1125 Sections 2 and/or 3 apply. Contact the Department at 23 323-4542 or (302) 739-9402 for additional information						
	Additional Information						
24.	Is There Any Additional Information Pertinent to this Application?   YES  NO						
If Y	'ES, complete the rest of Question 24.						
24.	1. Describe:						

#### Pellet Cooler Cyclone #1 EU 54

Pellet Mill #150Pellet Cooler (t/hr):50Hours/day of operation:24PM 10 factor (table 9.9.1-2)(#/ton feed):0.075

Note: PM 10 factor: .5\* 0.15 for high eff. Cyclone per table 9.9.1-2 PM 10= 0.075 #/ton \* 50 t/hr \* 8760 hr/yr \* T/2000 #= tpy PM 10

#### Pellet Cooler Cyclone #1 (using maximum hours)

Pollutant	Emission Factor (#/ton)	Hourly Emissions (lb/hr)	PTE (tons/yr)
PM	0.15	7.5	32.85
PM-10	0.075	3.75	16.425

Table 9.9 1-2 PARTICULATE EMISSION FACTORS FOR GRAIN PROCESSING FACILITIES<sup>a</sup>

			Filteral	ble <sup>b</sup>		Condensible PM <sup>c</sup>			
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Animal feed mills Grain receiving (SCC 3-02-008-02)	None	0.017°	Е	0.0025°	Е				
Grain cleaning (SCC 3-02-008-07)	Cyclone	<b>(f)</b>		(f)					
Storage	None	ND		ND					
Grain milling (SCC 3-02-008-15)									
Hammermill (SCC 3-02-008-17)	Cyclone	0.067 <sup>h</sup>	Е	(g)					
(500 5-02-000-17)	Baghouse	0.012 <sup>j</sup>	Е	(y)					
Flaker (SCC 3-02-008-18)	Cyclone	0.15 <sup>k</sup>	Е	(g)					
Grain cracker (SCC 3-02-008-19)	Cyclone	0.024 <sup>k</sup>	Е	(g)			i		
Mixer	None	ND		ND					
Conditioning	None	ND		ND					
Pelletizing Pellet cooler <sup>m</sup> (SCC 3-02-008-16)	Cyclone	0.36 <sup>n</sup>	E	(g)				0.059 <sup>p</sup>	Е
(SCC 3-02-008-10)	High efficiency cyclone'	0.15 <sup>q</sup>	Е	(g)					
Feed shipping (SCC 3-02-008-03)	None	0.0033°	Е	0.0008°	Е				
Wheat flour mills Grain receiving (SCC 3-02-007-31)	None	<b>(f)</b>		(f)					
Grain handling (SCC 3-02-007-32) (legs, belts, etc.)	None	(f)		(f)					

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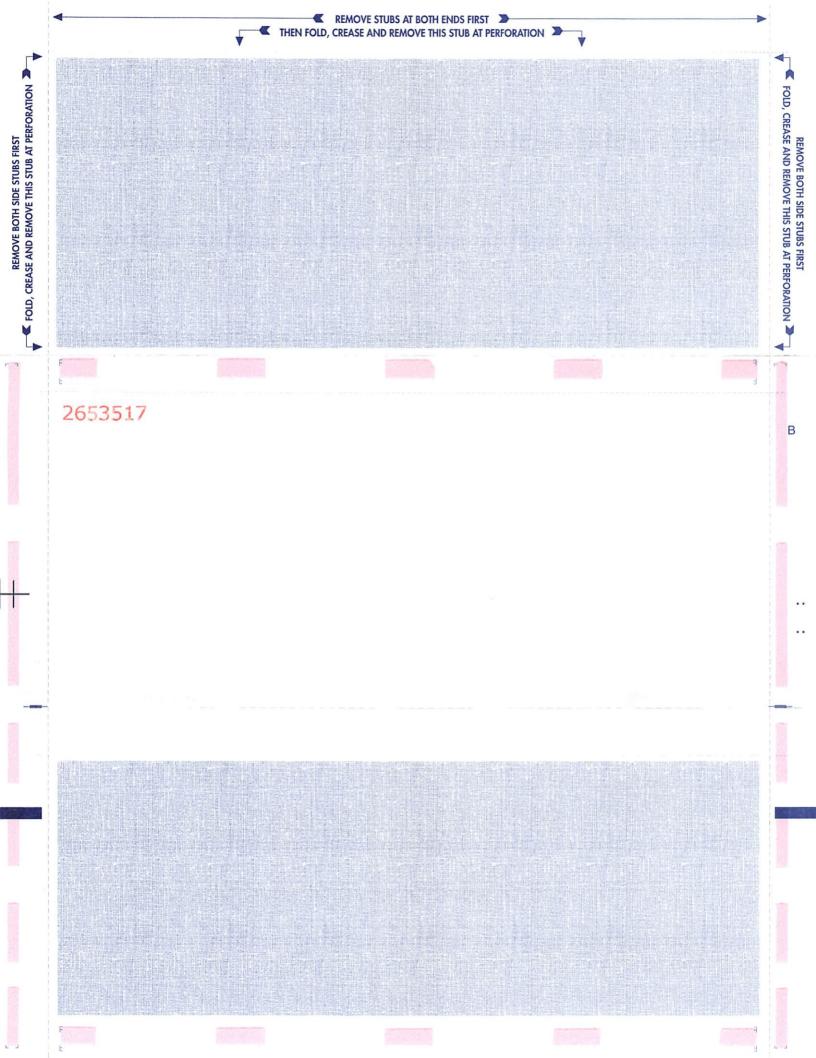
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# **ATTACHMENT 2**

GENERAL PROCESS FLOW DIAGRAM

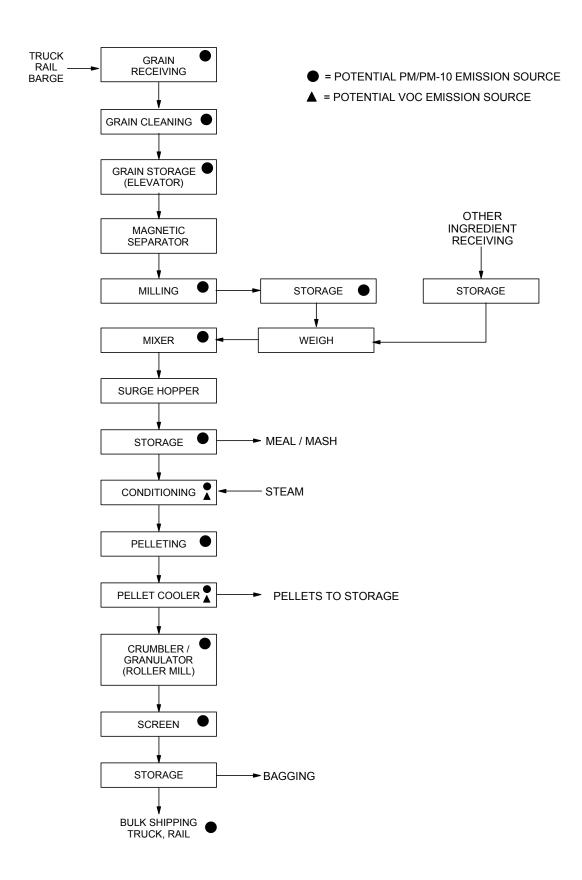


Figure 9.9.1-6. Typical animal feed milling process flow diagram.



## **ATTACHMENT 3**

EPA AP-42 CHAPTER 9.9.1 GRAIN ELEVATORS AND PROCESSES

#### 9.9.1 Grain Elevators And Processes

## 9.9.1.1 Process Description<sup>1-14</sup>

Grain elevators are facilities at which grains are received, stored, and then distributed for direct use, process manufacturing, or export. They can be classified as either "country" or "terminal" elevators, with terminal elevators further categorized as inland or export types. Operations other than storage, such as cleaning, drying, and blending, often are performed at elevators. The principal grains and oilseeds handled include wheat, corn, oats, rice, soybeans, and sorghum.

Country elevators are generally smaller elevators that receive grain by truck directly from farms during the harvest season. These elevators sometimes clean or dry grain before it is transported to terminal elevators or processors. Terminal elevators dry, clean, blend, and store grain before shipment to other terminals or processors, or for export. These elevators may receive grain by truck, rail, or barge, and generally have greater grain handling and storage capacities than do country elevators. Export elevators are terminal elevators that load grain primarily onto ships for export.

Regardless of whether the elevator is a country or terminal, there are two basic types of elevator design: traditional and modern. Traditional grain elevators are typically designed so the majority of the grain handling equipment (e.g., conveyors, legs, scales, cleaners) are located inside a building or structure, normally referred to as a headhouse. The traditional elevator often employs belt conveyors with a movable tripper to transfer the grain to storage in concrete or steel silos. The belt and tripper combination is located above the silos in an enclosed structure called the gallery or bin deck. Grain is often transported from storage using belt conveyors located in an enclosed tunnel beneath the silos. Particulate emissions inside the elevator structure may be controlled using equipment such as cyclones, fabric filters, dust covers, or belt wipers; grain may be oil treated to reduce emissions. Controls are often used at unloading and loading areas and may include cyclones, fabric filters, baffles in unloading pits, choke unloading, and use of deadboxes or specially designed spouts for grain loading. The operations of traditional elevators are described in more detail in Section 2.2.1. Traditional elevator design is generally associated with facilities built prior to 1980.

Country and terminal elevators built in recent years have moved away from the design of the traditional elevators. The basic operations performed at the elevators are the same; only the elevator design has changed. Most modern elevators have eliminated the enclosed headhouse and gallery (bin decks). They employ a more open structural design, which includes locating some equipment such as legs, conveyors, cleaners, and scales, outside of an enclosed structure. In some cases, cleaners and screens may be located in separate buildings. The grain is moved from the unloading area using enclosed belt or drag conveyors and, if feasible, the movable tripper has been replaced with enclosed distributors or turn-heads for direct spouting into storage bins and tanks. The modern elevators are also more automated, make more use of computers, and are less labor-intensive. Some traditional elevators have also been partially retrofitted or redesigned to incorporate enclosed outside legs, conveyors, cleaners, and other equipment. Other techniques used to reduce emissions include deepening the trough of the openbelt conveyors and slowing the conveyor speed, and increasing the size of leg belt buckets and slowing leg velocity. At loading and unloading areas of modern elevators, the controls cited above for traditional elevators can also be used to reduce emissions.

The first step at a grain elevator is the unloading of the incoming truck, railcar, or barge. A truck or railcar discharges its grain into a hopper, from which the grain is conveyed to the main part of the

elevator. Barges are unloaded by a bucket elevator (either a continuous barge unloader or marine leg) that is extended down into the barge hold. The main building at an elevator, where grain is elevated and distributed, is called the "headhouse". In the headhouse, grain is lifted on one of the elevator legs and, at older facilities, is typically discharged onto the gallery belt, which conveys the grain to the storage bins. A "tripper" diverts grain off the belt and into the desired bin. At more modern facilities, other modes of transfer include enclosed conveyors, direct spouting, augers, and screw conveyors. Grain is often cleaned, dried, and cooled for storage. Once in storage, grain may be transferred one or more times to different storage bins or may be emptied from a bin, treated or dried, and stored in the same or a different bin. The most common method for unloading ships is by leg, using either an in-house leg operated by the facility or a self-unloading system (leg and conveyors) designed into the vessel. Figure 9.9.1-1 presents the major process operations at a grain elevator.

A grain processing plant or mill receives grain from an elevator and performs various manufacturing steps that produce a finished food product. The grain receiving and handling operations at processing plants and mills are basically the same as at grain elevators. Examples of processing plants are flour mills, oat mills, rice mills, dry corn mills, and animal feed mills. The following subsections describe the processing of the principal grains. Additional information on grain processing may be found in AP-42 Section 9.9.2, Cereal Breakfast Food, and AP-42 Section 9.9.7, Corn Wet Milling.

## 9.9.1.1.1 Flour Milling<sup>2,5</sup> -

Most flour mills produce wheat flour, but durum wheat and rye are also processed in flour mills. The wheat flour milling process consists of 5 main steps: (1) grain reception, preliminary cleaning, and storage; (2) grain cleaning; (3) tempering or conditioning; (4) milling the grain into flour and its byproducts; and (5) storage and/or shipment of finished product. A simplified diagram of a typical flour mill is shown in Figure 9.9.1-2. Wheat arrives at a mill and, after preliminary cleaning, is conveyed to storage bins. As grain is needed for milling, it is withdrawn and conveyed to the mill area where it first enters a separator (a vibrating screen), then, an aspirator to remove dust and lighter impurities, and then passes over a magnetic separator to remove iron and steel particles. From the magnetic separator, the wheat enters a disc separator designed to catch individual grains of wheat and reject larger or smaller material and then to a stoner for removal of stones, sand, flints, and balls of caked earth or mud. The wheat then moves into a scourer which buffs each kernel and removes more dust and loose bran (hull or husk). Following the scouring step, the grain is sent to the tempering bins where water is added to raise the moisture of the wheat to make it easier to grind. When the grain reaches the proper moisture level, it is passed through an impact machine as a final cleaning step. The wheat flows into a grinding bin and then into the mill itself.

The grain kernels are broken open in a system of breaks by sets of corrugated rolls, each set taking feed from the preceding one. After each break, the grain is sifted. The sifting system is a combination of sieving operations (plansifters) and air aspiration (purifiers). The flour then passes through the smooth reducing rolls, which further reduce the flour-sized particles and facilitate the removal of the remaining bran and germ particles. Plansifters are used behind the reducing rolls to divide the stock into over-sized particles, which are sent back to the reducing rolls, and flour, which is removed from the milling system. Flour stock is transported from the milling system to bulk storage bins and subsequently packaged for shipment.

Generally, durum wheat processing comprises the same steps as those used for wheat flour milling. However, in the milling of durum, middlings rather than flour are the desired product. Consequently, the break system, in which middlings are formed, is emphasized over the part of the reduction system in which flour is formed. Grain receiving, cleaning, and storage are essentially

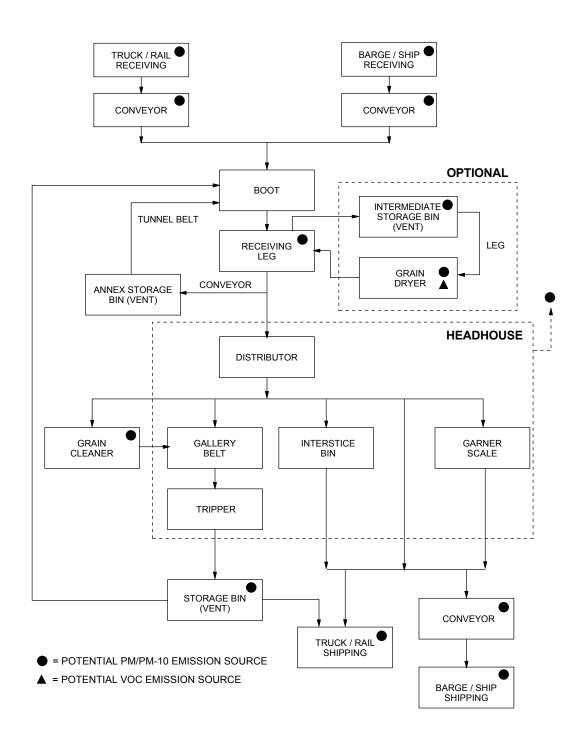


Figure 9.9.1-1. Major process operations at a grain elevator.

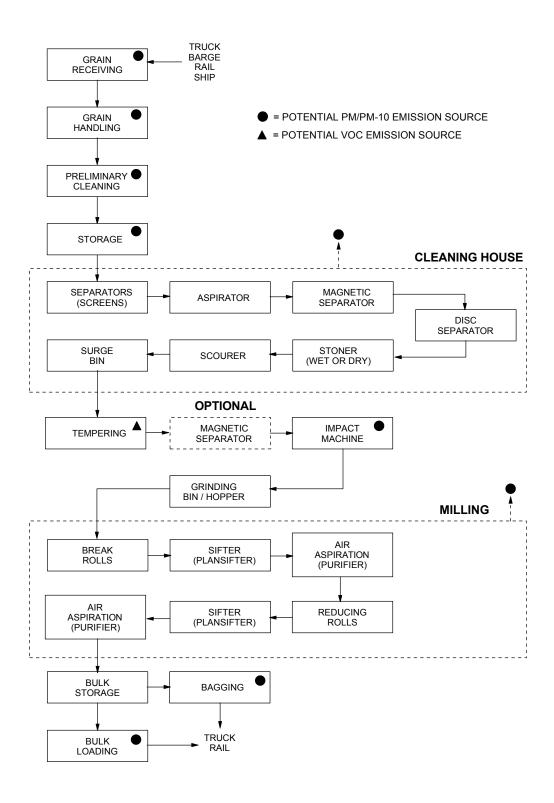


Figure 9.9.1-2. Simplified process flow diagram of a typical flour mill.

identical for durum and flour milling. The tempering step varies only slightly between the two processes. The tempering of durum uses the same equipment as wheat, but the holding times are shorter. Only the grain milling step differs significantly from the comparable flour milling step.

The break system in a durum mill generally has at least five sets of rolls for a gradual reduction of the stock to avoid producing large amounts of break flour. The rolls in the reduction system are used for sizing only, and not to produce flour. The sizing produces a uniform product for sale. The sifting system differs from that in a wheat flour mill in that it relies heavily on purifiers. In place of plansifters, conventional sieves are more common and are used to make rough separations ahead of the purifiers.

Rye milling and wheat flour milling are quite similar processes. The purpose of both processes is to make flour that is substantially free of bran and germ. The same basic machinery and process are employed. The flow through the cleaning and tempering portions of a rye mill is essentially the same as the flow through the wheat flour mill. However, because rye is more difficult to clean than wheat, this cleaning operation must be more carefully controlled.

In contrast to wheat milling, which is a process of gradual reduction with purification and classification, rye milling does not employ gradual reduction. Both the break and reduction roller mills in a rye mill are corrugated. Following grinding, the screening systems employ plansifters like those used in wheat flour mills. There is little evidence of purifier use in rye mills.

The wheat milling and rye milling processes are very similar because flour is the product of the break rolling system. In durum wheat flour milling, the intent is to produce as little flour as possible on the break rolls. As in wheat flour milling, the intent in rye milling is to make as much rye flour as possible on the break rolls. Consequently, there are more break rolls in proportion to reduction rolls in a rye mill than in a durum wheat flour mill.

## 9.9.1.1.2 Oat Milling $^{2,7}$ -

The milling process for oats consists of the following steps: (1) reception, preliminary cleaning, and storage; (2) cleaning; (3) drying and cooling; (4) grading and hulling; (5) cutting; (6) steaming; and (7) flaking. A simplified flow diagram of the oat milling process is shown in Figure 9.9.1-3. The receiving and storage operations are comparable to those described for grain elevators and for the wheat flour milling process. Preliminary cleaning removes coarse field trash, dust, loose chaff, and other light impurities before storage. After the oats are removed from storage, they flow to a milling separator combining coarse and fine screening with an efficient aspiration. In the next sequence of specialized cleaning operations, the oats are first routed to a disk separator for stick removal, and then are classified into three size categories. Each size category is subjected to a variety of processes (mechanical and gravitational separation, aspiration, and magnetic separation) to remove impurities. Large and short hulled oats are processed separately until the last stages of milling.

The next step in the oat processing system is drying and cooling. Oats are dried using pan dryers, radiator column dryers, or rotary steam tube dryers. Oats typically reach a temperature of 88° to 98°C (190° to 200°F) here, and the moisture content is reduced from 12 percent to 7 to 10 percent. After drying and cooling, the oats are ready for hulling; hulled oats are called groats. Some mills are now hulling oats with no drying or conditioning, then drying the groats separately to develop a toasted flavor. Hulling efficiency can be improved by prior grading or sizing of the oats. The free hulls are light enough that aspirators remove them quite effectively.

Generally, the final step in the large oat system is the separation of groats totally free of whole oats that have not had the hulls removed. These groats bypass the cutting operation and are directed to

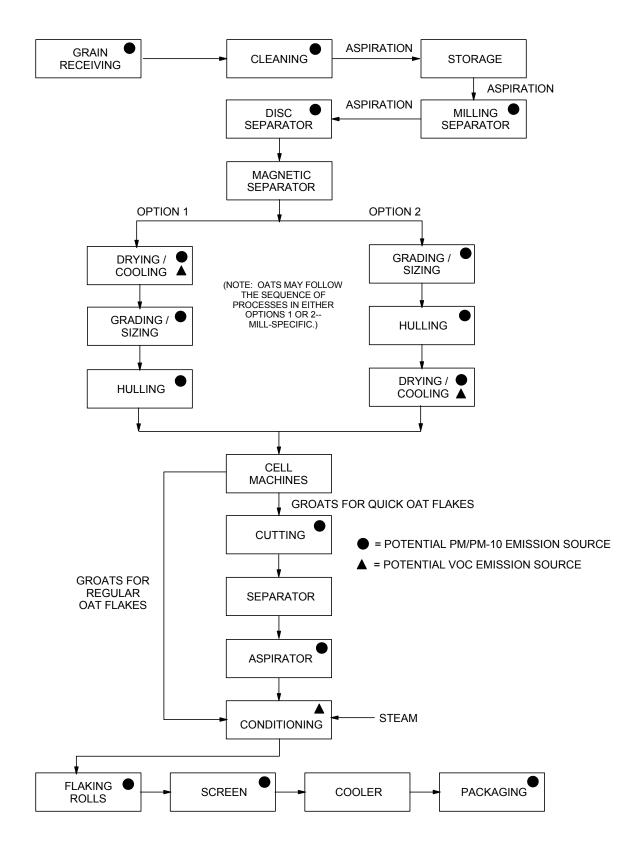


Figure 9.9.1-3. Flow diagram for oat processing operations.<sup>8</sup>

storage prior to flaking. The rejects are sent to the cutting plant. The cutting plant is designed to convert the groats into uniform pieces while producing a minimum of flour. The cut material is now ready for the flaking plant. First, the oats are conditioned by steaming to soften the groats thereby promoting flaking with a minimum of breakage. The steamed groats pass directly from the steamer into the flaking rolls. Shakers under the rolls remove fines and overcooked pieces are scalped off. The flakes generally pass through a dryer and cooler to quickly reduce moisture content and temperature which ensures acceptable shelf life. The cooled flakes are then conveyed to the packaging system.

## 9.9.1.1.3 Rice Milling<sup>2,8-10</sup>-

The first step in rice processing after harvest is drying using either fixed-bed or continuous-flow dryers to reduce the wet basis moisture content (MCwb) from 24 to 25 percent to 13 to 14 percent MCwb. Essentially all of the rice is dried either on the farm or at commercial drying facilities prior to shipping to the rice mill. After the rice is dried, it is stored and subsequently shipped to either conventional or parboil rice mills for further processing. There are three distinct stages in both mills: (1) rough rice receiving, cleaning, drying, and storage; (2) milling; and (3) milled rice and byproduct bagging, packaging, and shipping. A simplified flow diagram of the rice milling process is shown in Figure 9.9.1-4.

Grain is received primarily by truck and rail. The rough rice is precleaned using combinations of scalpers, screens, aspirators, and magnetic separators and then passed through a stoner, or gravity separator, to remove stones from the grain. The cleaned rice is transported to a disk huller where the rice is dehulled. The rice then passes through a sieve to remove bran and small brokens and to an aspirator to remove hulls. The unshelled rice grains (commonly called paddy) and brown rice are separated in a paddy separator. The unshelled paddy is then fed into another pair of shellers set closer together than the first set, and the process of shelling, aspiration, and separation is repeated.

From the paddy machines, the rice is conveyed to a sequence of milling machines called whitening cones, which scour off the outer bran coats and the germ from the rice kernels. Milling may be accomplished by a single pass through a mill or by consecutive passages through multiple whitening cones. The discharge from each stage is separated by a sieve. After the rice is milled, it passes through a polishing cone, which removes the inner bran layers and the proteinaceous aleurone layer. Because some of the kernels are broken during milling, a series of classifiers, known as trieurs, is used to separate the different size kernels. The rice may be sold at this point as polished, uncoated rice, or it may be conveyed to machines known as trumbels, in which the rice is coated with talc and glucose to give the surface a gloss. The rice is transferred to bulk storage prior to packing and shipping. For packing, the rice is transported to a packing machine where the product is weighed and placed in burlap sacks or other packaging containers.

In parboiling mills, the cleaned rough rice is steamed and dried prior to the milling operations. Pressure vessels are used for the steaming step, and steam tube dryers are used to dry the rice to 11 to 13 percent MCwb. Following the drying step, the rice is milled in conventional equipment to remove hull (bran), and germ.

## 9.9.1.1.4 Corn Dry Milling<sup>2,12-13</sup> -

Corn is dry milled by either a degerming or a nondegerming system. Because the degerming system is the principal system used in the United States, it will be the focus of the dry corn milling process description here. A simplified flow diagram of the corn dry milling process is shown in Figure 9.9.1-5. The degerming dry corn milling process is more accurately called the tempering degerminating (TD) system. The degerming system involves the following steps after receiving the grain: (1) dry cleaning, and if necessary, wet cleaning; (2) tempering; (3) separation of hull, germ, and

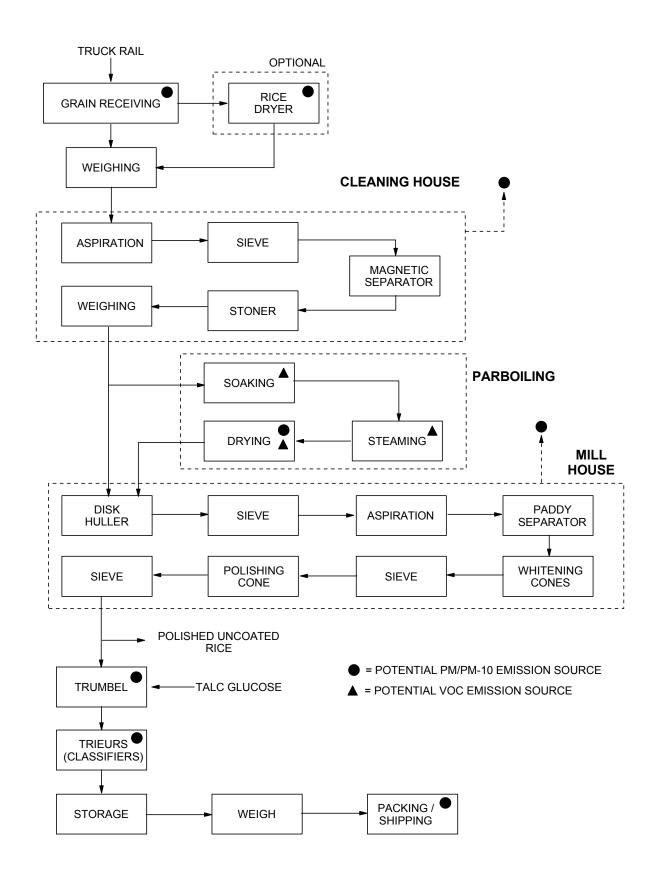


Figure 9.9.1-4. Flow diagram for conventional and parboil rice mills.

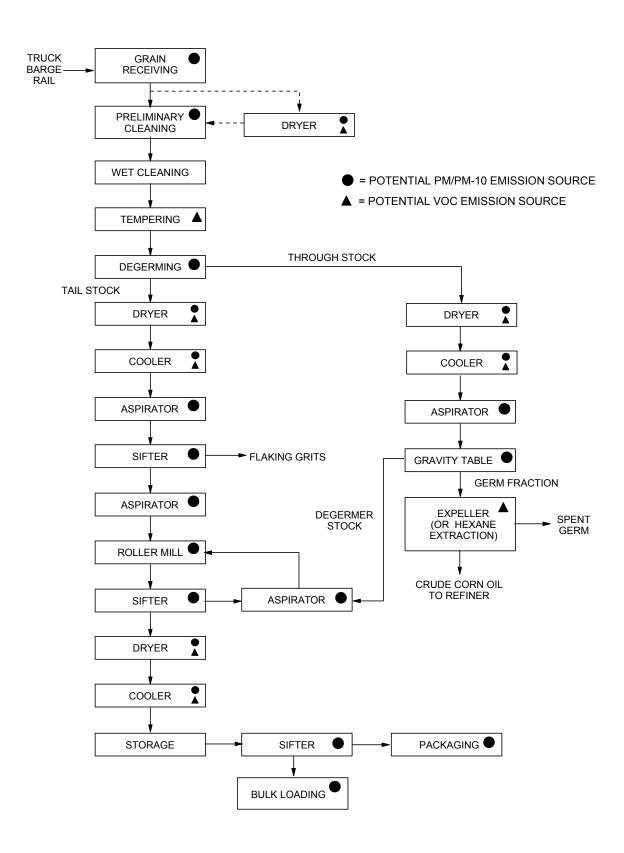


Figure 9.9.1-5. Simplified process flow diagram for a corn dry milling operation with degerming.

tip cap from the endosperm in the degerminator; (4) drying and cooling of degermer product; (5) multistep milling of degermer product through a series of roller mills, sifters, aspirators, and purifiers; (6) further drying of products, if necessary; (7) processing of germ fraction for recovery of crude corn oil; and (8) packaging and shipping of products.

Unloading and dry cleaning of corn is essentially the same as described for wheat. However, for corn, surface dirt and spores can best be removed by wet cleaning, which involves a washing-destoning unit followed by a mechanical dewatering unit. After cleaning, the corn is sent through the tempering or conditioning step, which raises the moisture content of the corn to 21 to 25 percent. After tempering, the corn is degermed, typically in a Beall degermer and corn huller. The Beall degermer is essentially an attrition device built in the form of a cone mill. The product exits in two streams, thru-stock and tail stock. Rotary steam-tube dryers are often used to dry the degermer product, because its moisture content must be in the 15 to 18 percent range for proper milling. After drying, the product is cooled to 32° to 37°C (90° to 100°F). After drying and cooling, the degermer stock is sifted or classified by particle size and is fed into the conventional milling system.

The milling section in a dry corn mill consists of sifting, classifying, milling, purifying, aspirating, and possibly, final drying operations. The feed to each pair of rolls consists of selected mill streams produced during the steps of sifting, aspirating, roller milling, and gravity table separating. For the production of specific products, various streams are withdrawn at appropriate points in the milling process. A number of process streams are often blended to produce a specific product. The finished products are stored temporarily in working bins, dried and cooled if necessary, and rebolted (sifted) before packaging or shipping in bulk.

Oil is recovered from the germ fraction either by mechanical screw presses or by a combination of screw presses and solvent extraction. A more detailed discussion of the corn oil extraction process is included in AP-42 Section 9.11.1, Vegetable Oil Processing.

## 9.9.1.1.5 Animal Feed Mills<sup>2,5,14</sup> -

The manufacture of feed begins with receiving of ingredients at the mill. A simplified flow diagram of the animal feed manufacturing process is shown in Figure 9.9.1-6. more than 200 ingredients may be used in feed manufacture, including grain, byproducts (e.g., meat meal, bone meal, beet and tomato pulp), and medicinals, vitamins, and minerals (used in very small portions). Grain is usually received at the mill by hopper bottom truck and/or rail cars, or in some cases, by barge. Most mills pass selected feed ingredients, primarily grains, through cleaning equipment prior to storage. Cleaning equipment includes scalpers to remove coarse materials before they reach the mixer. Separators, which perform a similar function, often consist of reciprocating sieves that separate grains of different sizes and textures. Magnets are installed ahead of the grinders and at other critical locations in the mill system to remove pieces of metal, bits of wire, and other foreign metallic matter, which could harm machinery and contaminate the finished feed. From the cleaning operation, the ingredients are directed to storage.

Upon removal from storage, the grain is transferred to the grinding area, where selected whole grains, primarily corn, are ground prior to mixing with other feed components. The hammermill is the most widely used grinding device. The pulverized material is forced out of the mill chamber when it is ground finely enough to pass through the perforations in the mill screen.

Mixing is the most important process in feed milling and is normally a batch process. Ingredients are weighed on bench or hopper scales before mixing. Mixers may be horizontal or vertical type, using either screws or paddles to move the ingredients. The material leaving the mixer is meal, or

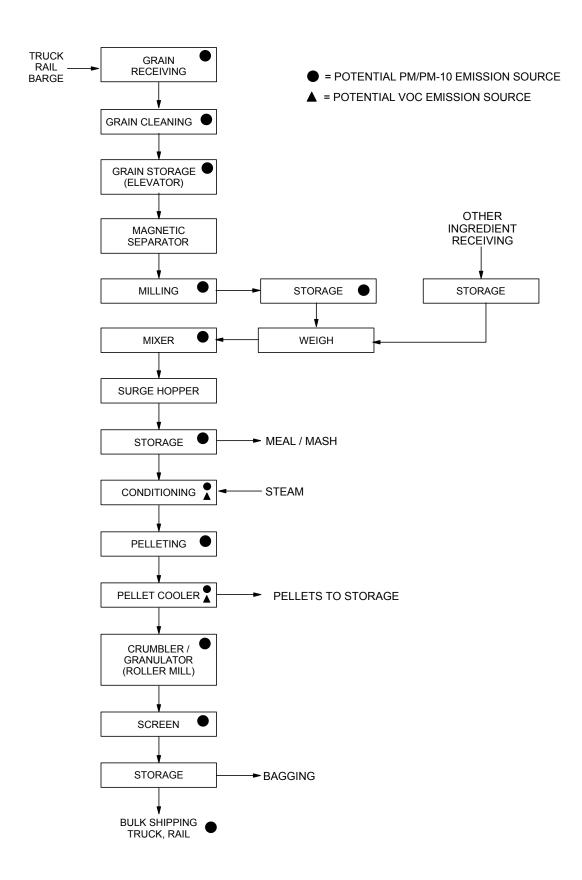


Figure 9.9.1-6. Typical animal feed milling process flow diagram.

mash, and may be marketed in this form. If pellets are to be made, the meal is conditioned with steam prior to being pelleted.

Pelleting is a process in which the conditioned meal is forced through dies. Pellets are usually 3.2 to 19 mm (1/8 to 3/4 in.) in diameter. After pelleting, pellets are dried and cooled in pellet coolers. If pellets are to be reduced in size, they are passed through a crumbler, or granulator. This machine is a roller mill with corrugated rolls. Crumbles must be screened to remove fines and oversized materials. The product is sent to storage bins and then bagged or shipped in bulk.

In modern feed mills, transport equipment is connected with closed spouting and turnheads, covered drag and screw conveyors, and tightly sealed transitions between adjoining equipment to reduce internal dust loss and consequent housekeeping costs. Also many older facilities have upgraded to these closed systems.

## 9.9.1.1.6 Malted Barley Production<sup>36-37</sup> -

Barley is shipped by railcar or truck to malting facilities. A screw conveyor or bucket elevator typically transports barley to storage silos or to the cleaning and sizing operations. The barley is cleaned and separated by size (using screens) and is then transferred to a malthouse where it is rinsed in steeping tanks (steeped) and is allowed to germinate. Following steeping and germination, "green" malt is dried, typically in an indirect-, natural gas-fired malt kiln. Malt kilns typically include multiple levels, called beds or layers. For a two-level kiln, green malt, with a moisture content of about 45 percent, enters the upper deck of the kiln and is dried, over a 24-hour period, to between 15 and 20 percent. The barley is then transferred to the lower deck of the kiln, where it is dried to about 4 percent over a second 24-hour period. Some facilities burn sulfur in a sulfur stove and exhaust the stove into the kiln at selected times during the kiln cycle. The sulfur dioxide serves as a fungicide, bactericide, and preservative. Malted barley is then transferred by screw conveyor to a storage elevator until it is shipped.

## 9.9.1.2 Emissions And Controls<sup>2,5,14-39</sup>

The main pollutant of concern in grain storage, handling, and processing facilities is particulate matter (PM). Organic emissions (e.g., hexane) from certain operations at corn oil extraction facilities may also be significant. These organic emissions (and related emissions from soybean and other oilseed processing) are discussed in AP-42 Section 9.11.1. Also, direct fired grain drying operations and product dryers in grain processing plants may emit small quantities of VOC's and other combustion products; no data are currently available to quantify the emission of these pollutants. The following sections focus primarily on PM sources at grain elevators and grain milling/processing facilities.

#### 9.9.1.2.1 Grain Elevators -

Except for barge and ship unloading and loading activities, the same basic operations take place at country elevators as at terminal elevators, only on a smaller scale and with a slower rate of grain movement. Emission factors for various grain elevator operations are presented later in this subsection. Because PM emissions at both types of elevators are similar, they will be discussed together in this subsection.

In trying to characterize emissions and evaluate control alternatives, potential PM emission sources can be classified into three groups. The first group includes external emission sources (grain receiving and grain shipping), which are characterized by direct release of PM from the operations to the atmosphere. These operations are typically conducted outside elevator enclosures or within partial enclosures, and emissions are quickly dispersed by wind currents around the elevator. The second group of sources are process emission sources that may or may not be vented to the atmosphere and include

grain cleaning and headhouse and internal handling operations (e.g., garner and scale bins, elevator legs, and transfer points such as the distributor and gallery and tunnel belts). These operations are typically located inside the elevator structure. Dust may be released directly from these operations to the internal elevator environment, or aspiration systems may be used to collect dust generated from these operations to improve internal housekeeping. If aspiration systems are used, dust is typically collected in a cyclone or fabric filter before the air stream is discharged to the atmosphere. Dust emitted to the internal environment may settle on internal elevator surfaces, but some of the finer particles may be emitted to the environment through doors and windows. For operations not equipped with aspiration systems, the quantity of PM emitted to the atmosphere depends on the tightness of the enclosures around the operation and internal elevator housekeeping practices. The third group of sources includes those processes that emit PM to the atmosphere in a well-defined exhaust stream (grain drying and storage bin vents). Each of these operations is discussed in the paragraphs below.

The amount of dust emitted during the various grain-handling operations may depend upon the type of grain being handled, the quality or grade of the grain, the moisture content of the grain, the speed of the belt conveyors used to transport the grain, and the extent and efficiency of dust containment systems (i.e., hoods, sheds, etc.) in use at an elevator. Part of the dust liberated during the handling of grain at elevators gets into the grain during the harvesting operation. However, most of these factors have not been studied in sufficient detail to permit the delineation of their relative importance to dust generation rates.

Grain dust emitted from grain elevator handling operations comprises about 70 percent organic material. The dust may include particles of grain kernels, small amounts of spores of smuts and molds, insect debris, pollens, and field dust. Data recently collected on worker exposure to grain dust indicate that the characteristics of the dust released from processing operations to the internal elevator environment vary widely. Because these dusts have a high organic content and a substantial suspendible fraction, concentrations above the minimum explosive concentration (MEC) pose an explosion hazard. Housekeeping practices instituted by the industry have reduced explosing hazards so this situation is rarely encountered in work areas.

Recent research on dust emissions from grain handling operations indicate that the fraction of dust particles equal to or less than 10 micrometers ( $\mu m$ ) in aerodynamic diameter (PM-10) averages approximately 25 percent of total PM, and the fraction of dust particles less than 2.5  $\mu m$  in aerodynamic diameter (PM-2.5) averages about 17 percent of PM-10.

Elevators in the United States receive grain by truck, railroad hopper car, and barge. The two principal factors that contribute to dust generation during bulk unloading are wind currents and dust generated when a falling stream of grain strikes the receiving pit. Falling or moving streams of grain initiate a column of air moving in the same direction. Grain unloading is an intermittent source of dust occurring only when a truck or car is unloaded. For country elevators it is a significant source during the harvest season and declines sharply or is nonexistent during other parts of the year. At terminal elevators, however, unloading is a year-round operation.

Trucks, except for the hopper (gondola) type, are generally unloaded by the use of some type of truck dumping platform. Hopper trucks discharge through the bottom of the trailer. Elevators are often designed with the truck unloading dump located in a drive-through tunnel. These drive-through areas are sometimes equipped with a roll-down door on one end, although, more commonly they are open at both ends so that the trucks can enter and leave as rapidly as possible. The drive-through access can act as a "wind-tunnel" in that the air may blow through the unloading area at speeds greater than the wind in the open areas away from the elevator. However, the orientation of the facility to the prevailing wind

direction can moderate this effect. Many facilities have installed either roll-down or bi-fold doors to eliminate this effect. The use of these doors can greatly reduce the "wind tunnel" effect and enhance the ability to contain and capture the dust.

The unloading pit at a grain elevator usually consists of a heavy grate approximately 3.05 m x 3.05 m (10 ft x 10 ft) through which the grain passes as it falls into the receiving pit. This pit will often be partially filled with grain as the truck unloads because the conveyor beneath the pit does not carry off the grain as fast as it enters. The dust-laden air emitted by the truck unloading operation results from displacement of air out of the pit plus the aspiration of air caused by the falling stream of grain. The dust itself is composed of field dirt and grain particles. Unloading grain from hopper trucks with choke flow-practices can provide a substantial reduction in dust emissions.

Similarly, a hopper railcar can be unloaded with minimal dust generation if the material is allowed to form a cone around the receiving grate (i.e., choke feed to the receiving pit). This situation will occur when either the receiving pit or the conveying system serving the pit is undersized in comparison to the rate at which material can be unloaded from the hopper car. In such cases, dust is generated primarily during the initial stage of unloading, prior to establishment of the choked-feed conditions. Dust generated by wind currents can be minimized by the use of a shed enclosed on two sides with a manual or motorized door on one end or a shroud around the hopper discharge.

In most cases, barges are unloaded by means of a retractable bucket type elevator that is lowered into the hold of the barge. There is some generation of dust in the hold as the grain is removed and also at the top of the leg where the grain is discharged onto the transfer belt. This latter source is more appropriately designated a transfer point.

The loadout of grain from elevators into railcar, truck, barge, or ship is another important source of PM emissions and is difficult to control. Gravity is usually used to load grain from bins above the loading station or from the scale in the headhouse. The main causes of dust emissions when loading bulk grain by gravity into trucks or railcars is the wind blowing through the loading sheds and dust generated when the falling stream of grain strikes the truck or railcar hopper. The grain leaving the loading spout is often traveling at relatively high velocity, and dead boxes, aspiration, socks, or other means are often used to reduce dust emissions. Dust emitted during loading of barges and ships is comparable to levels generated during loading of trucks or railcars. The openings for the holds in ocean-going vessels may also be covered with tarps if needed to meet air quality standards.

Grain dryers present a difficult problem for air pollution control because of the large volumes of air exhausted from the dryer, the large cross-sectional area of the exhaust, the low specific gravity of the emitted dust, and the high moisture content of the exhaust stream. The rate of emission of PM from grain dryers is primarily dependent upon the type of grain, the dustiness of the grain, and the dryer configuration (rack or column type). The particles emitted from the dryers, although relatively large, may be very light and difficult to collect. However, during corn drying, the characteristic "bees wing" is emitted along with normal grain dust. "Bees wing," a light flaky material that breaks off from the corn kernel during drying and handling, is a troublesome PM emission. Essentially, all bees wing emissions are more than 50  $\mu$ m in diameter, and the mass mean diameter is probably in the region of 150  $\mu$ m. In addition to the bees wings, the dust discharged from grain dryers consists of hulls, cracked grain, weed seeds, and field dust. Effluent from a corn dryer may consist of 25 percent bees wing, which has a specific gravity of about 0.70 to 1.2. Approximately 95 percent of the grain dust is larger than 50  $\mu$ m.

Cross-flow column dryers have a lower emission rate than rack dryers because some of the dust is trapped by the column of grain. In some cases, an enclosure may be built around the dryer that can act

as a relatively effective settling chamber because of its moist environment. New grain dryers being sold today do not require the use of enclosures. In rack dryers drying corn, the emission rate for larger PM can be higher because the turning motion of the grain liberates more bees wings from the kernel, and the design facilitates dust escape. Some rack dryers are exhausted only from one or two points and are thus better suited for control device installation. The EPA's New Source Performance Standards (NSPS) for grain elevators established visible emission limits for grain dryers by requiring 0 percent opacity for emissions from column dryers and rack dryers. The NSPS zero opacity standard does not apply to column dryers with column plate perforations less than or equal to 2.4 mm in diameter (0.094 in.) or to rack dryers with a screen filter that has openings that are less than or equal to 50 mesh.

Equipment used to clean grain varies from simple screening devices to aspiration-type cleaners. Both types of systems potentially generate substantial quantities of PM depending on the design and extent of enclosure.

Both country and terminal elevators are usually equipped with garner and scale bins for weighing of grain. A country elevator may have only one garner bin and scale bin. However, a terminal elevator has multiple scale and garner bin systems, each with a capacity ranging from 42.3 to 88.1 m³ (1,200 to 2,500 bu) to process 1,233 to 2,643 m³/hr (35,000 to 75,000 bu/hr). Dust may be emitted from both the scale and garner bin whenever grain is admitted. The incoming stream of grain displaces air from the bin, and the displaced air entrains dust. The potential for emissions depends on the design of the system. For example, some facilities employ a relief duct that connects the two pieces of equipment to provide a path for displaced air. Also, in some cases, the bins are completely open at the top while some systems are completely enclosed.

The leg may be aspirated to remove dust created by the motion of the buckets and the grain flow. A variety of techniques are used to aspirate elevator legs. For example, some are aspirated at both the top and bottom; others are fitted with ducting from the top to the bottom in order to equalize the pressure, sometimes including a small blower to serve this purpose. The collected dust is discharged to a cyclone or filter. Leg vents may emit small amounts of dust under some operating conditions. However, these vents are often capped or sealed to prevent dust emissions. The sealing or capping of the vent is designed to act as an explosion relief vent after a certain internal pressure is reached to prevent damage to the equipment.

When grain is handled, the kernels scrape and strike against each other and the conveying medium. This action tends to rub off small particles of chaff and to fragment some kernels. Dust is continuously generated, and the grain is never absolutely clean. Belt conveyors have less rubbing friction than either screw or drag conveyors, and therefore, generate less dust. Dust emissions usually occur at belt transfer points as materials fall onto or away from a belt. Belt speed has a strong effect on dust generation at transfer points. Examples of transfer points are the discharge from one belt conveyor or the discharge from a bin onto a tunnel belt.

Storage bin vents, which are small screen-covered openings located at the top of the storage bins, are used to vent air from the bins as the grain enters. The grain flow into a bin induces a flow of air with the grain, and the grain also displaces air out of the bin. The air pressure that would be created by these mechanisms is relieved through the vents. The flow of grain into the bin generates dust that may be carried out with the flow of air through the bin vents. The quantity of dust released through the vents increases as the level of the grain in the bin increases. Bin vents are common to both country and terminal elevators, although the quantity of dust emitted is a function of the grain handling rate, which is considerably higher in terminal elevators.

The three general types of measures that are available to reduce emissions from grain handling and processing operations are process modifications designed to prevent or inhibit emissions, capture/collection systems, and oil suppression systems that inhibit release of dust from the grain streams. The following paragraphs describe the general approaches to process controls, capture systems, and oil suppression. The characteristics of the collection systems most frequently applied to grain handling and processing plants (cyclones and fabric filters) are then described, and common operation and maintenance problems found in the industry are discussed.

Because emissions from grain handling operations are generated as a consequence of mechanical energy imparted to the dust by the operations themselves and local air currents in the vicinity of the operations, an obvious control strategy is to modify the process or facility to limit the effects of those factors that generate emissions. The primary preventive measures that facilities have used are construction and sealing practices that limit the effect of air currents and minimizing grain free fall distances and grain velocities during handling and transfer. Some construction and sealing practices that minimize emissions are enclosing the receiving area to the degree practicable, preferably with doors at both ends of a receiving shed; specifying dust-tight cleaning and processing equipment; using lip-type shaft seals at bearings on conveyor and other equipment housings; using flanged inlets and outlets on all spouting, transitions, and miscellaneous hoppers; and fully enclosing and sealing all areas in contact with products handled.

A substantial reduction in emissions from receiving, shipping, handling, and transfer areas can be achieved by reducing grain free fall distances and grain velocities. Choke unloading reduces free fall distance during hopper car unloading. The same principle can be used to control emissions from grain transfer onto conveyor belts and from loadout operations. An example of a mechanism that is used to reduce grain velocities is a "dead box" spout, which is used in grain loadout (shipping) operations. The dead box spout slows down the flow of grain and stops the grain in an enclosed area. The dead box is mounted on a telescoping spout to keep it close to the grain pile during operation. In principle, the grain free falls down the spout to an enclosed impact dead box, with grain velocity going to zero. It then falls onto the grain pile. Typically, the entrained air and dust liberated at the dead box is aspirated back up the spout to a dust collector. Finally, several different types of devices are available that, when added to the end of the spout, slow the grain flow and compress the grain discharge stream. These systems entrap the dust in the grain stream, thereby providing a theoretical reduction in PM emissions. There are few, if any, test data from actual ship or barge loading operations to substantiate this theoretical reduction in emissions.

While the preventive measures described above can minimize emissions, most facilities also require ventilation, or capture/collection, systems to reduce emissions to acceptable levels. In fact, air aspiration (ventilation) is a part of the dead box system described above. Almost all grain handling and processing facilities, except relatively small grain elevators, use capture/collection on the receiving pits, cleaning operations, and elevator legs. Generally, milling and pelletizing operations at processing plants are ventilated, and some facilities use hooding systems on all handling and transfer operations.

Grain elevators that rely primarily on aspiration typically duct many of the individual dust sources to a common dust collector system, particularly for dust sources in the headhouse. Thus, aspiration systems serving elevator legs, transfer points, bin vents, etc., may all be ducted to one collector in one elevator and to two or more individual systems in another. Because of the myriad possibilities for ducting, it is nearly impossible to characterize a "typical" grain elevator from the standpoint of delineating the exact number and types of air pollution sources and the control configurations for those sources.

The control devices typically used in the grain handling and processing industry are cyclones (or mechanical collectors) and fabric filters. Cyclones are generally used only on country elevators and small processing plants located in sparsely populated areas. Terminal elevators and processing plants located in densely populated areas, as well as some country elevators and small processing plants, normally use fabric filters for control. Both of these systems can achieve acceptable levels of control for many grain handling and processing sources. Although cyclone collectors can achieve acceptable performance in some scenarios, and fabric filters are highly efficient, both devices are subject to failure if they are not properly operated and maintained. Also, malfunction of the ventilation system can lead to increased emissions at the source.

The emission control methods described above rely on either process modifications to reduce dust generation or capture collection systems to control dust emissions after they are generated. An alternative control measure that has developed over the last 10 years is dust suppression by oil application. The driving forces for developing most such dust suppression systems have been grain elevator explosion control as well as emission control. Consequently, few data have been published on the amount of emission reduction achieved by such systems. Recent studies, however, have indicated that a PM reduction of approximately 60 to 80 percent may be achievable (see References 57 and 61 in Section 4 of the Background Report).

Generally, these oil application dust suppression systems use either white mineral oil, soybean oil, or some other vegetable oil. Currently the Food and Drug Administration restricts application rates of mineral oil to 0.02 percent by weight. Laboratory testing and industry experience have shown that oil additives applied at a rate of 60 to 200 parts per million by weight of grain, or 0.5 to 1.7 gallons of oil per thousand bushels of grain can provide effective dust control.<sup>39</sup> The effectiveness of the oil suppression system depends to some extent on how well the oil is dispersed within the grain stream after it is applied. Several options are available for applying oil additives.

- 1. As a top dressing before grain enters the bucket elevator or at other grain transfer points.
- 2. From below the grain stream at a grain transfer point using one or more spray nozzles.
- 3. In the boot of the bucket elevator leg.
- 4. At the discharge point from a receiving pit onto a belt or other type conveyor.
- 5. In a screw conveyor.

#### 9.9.1.2.2 Grain Processing Plants -

Several grain milling operations, such as receiving, conveying, cleaning, and drying, are similar to those at grain elevators. In addition, applications of various types of grinding operations to the grain, grain products, or byproducts are further sources of emissions. The hammermill is the most widely used grinding device at feed mills. Some product is recovered from the hammermill with a cyclone collector or baghouse. Mills, similar to elevators, use a combination of cyclones and fabric filters to conserve product and to control emissions. Several types of dryers are used in mills, including the traditional rack or column dryers, fluidized bed dryers (soybean processing), and flash-fired or direct-fired dryers (corn milling). These newer dryer types might have lower emissions, but data are insufficient at this time to quantify the difference. The grain precleaning often performed before drying also likely serves to reduce emissions.

Because of the operational similarities, emission control methods used in grain milling and processing plants are similar to those in grain elevators. Cyclones or fabric filters are often used to control emissions from the grain handling operations (e. g., unloading, legs, cleaners, etc.) and also from other processing operations. Fabric filters are used extensively in flour mills. However, certain operations within milling operations are not amenable to the use of these devices and alternatives are

needed. Wet scrubbers, for example, are applied where the effluent gas stream has a high moisture content. A few operations have been found to be difficult to control by any method. Various emission control systems have been applied to operations within the grain milling and processing industry.<sup>2</sup>

Grain processing facilities also have the potential to emit gaseous pollutants. Natural gas-fired dryers and boilers are potential sources of combustion byproducts and VOC. The production of various modified starches has the potential for emissions of hydrochloric acid or ethylene oxide. However, no data are available to confirm or quantify the presence of these potential emissions. Neither are there any data available concerning the control of these potential emissions.

Table 9.9.1-1 presents emission factors for filterable PM and PM-10 emissions from grain elevators. Table 9.9.1-2 presents emission factors for filterable PM; PM-10; inorganic, organic and total condensible PM emissions from grain processing facilities.

The most recent source test data for grain elevators either does not differentiate between country and inland terminal elevators or does not show any significant difference in emission factors between these two types of elevators. There are no current emission source test data for export terminal elevators. Because there is no significant difference in emission factors between different types of elevators, the emission factors presented in Table 9.9.1-1 are for grain elevators, without any distinction between elevator types.

In Tables 9.9.1-1 and 9.9.1-2, a number of potential emission sources are presented for each type of facility. The number and type of processes that occur within a specific elevator or grain processing plant will vary considerably from one facility to another. The total emissions from a specific facility will be dependent upon the different types of processes and the number of times a process or operation occurs within each facility. Not all processes occur at every facility; therefore, the specific emission sources and number of sources must be determined for each individual facility. It is not appropriate to sum emission factors for all sources and assume that total factor for all facilities.

#### 9.9.1.3 Example Use of Emission Factor Table

The emission factors in Table 9.9.1-1 predict emissions from different operations at grain handling facilities. Except where specifically noted in the tables, the factors predict uncontrolled emissions.

The following guidance (with illustrative examples) is provided to users to promote greater consistency in the application of the data in Table 9.9.1-1.

(1) The emission factors for grain receiving and grain shipping (e.g., rail, truck, barge and/or ship) should be applied to the total amount of grain received and/or shipped by that mode of transportation.

Example: Facility reports shipping 1 million tons of grain by vessel. The calculated uncontrolled PM-10 emissions are:

 $1,000,000 \text{ tons } \times 0.012 \text{ lbs/ton} = 12,000 \text{ lbs or } 6 \text{ tons of PM-}10$ 

Example: Facility reports receiving 2 million tons of grain using a continuous barge unloader (e.g., Heyl-Patterson or Link Belt). The calculated uncontrolled PM-10 emissions are:

 $2,000,000 \text{ tons } \times 0.0073 \text{ lbs/ton} = 14,600 \text{ lbs or } 7.3 \text{ tons of PM-10}$ 

(2) Truck receiving can represent a unique situation at grain handling facilities. The preponderance of grain facilities receive grain by both straight and hopper bottom trucks. When actual truck counts/receipts by type of truck are not known, the emission factor for trucks should represent a weighted-average or a conservative percentage of the distribution of straight and hopper bottom trucks normally handled at the facility, or at a similar facility. The use of hopper bottom trucks to haul grain is steadily increasing over time. In some cases, industry reports that receipts of grain by hopper bottom trucks can often exceed 75 percent and in some cases represent nearly 100 percent of truck receipts. Thus, exclusive reliance on the emission factor for straight trucks would normally result in emission estimates that are strongly biased high.

Example: Facility reports receiving 42,000 tons of grain by truck with 75% being hopper bottom trucks and 25% straight trucks. The weighted average PM-10 emission factor for this facility is:

```
0.75 \times 0.0078 \text{ lbs/ton} = 0.006 \text{ lbs/ton}

0.25 \times 0.059 \text{ lbs/ton} = 0.015 \text{ lbs/ton}

Weighted average = 0.021 lbs/ton
```

Using this factor, the calculated uncontrolled PM-10 emissions from the truck dump can be calculated:

```
0.021 lbs/ton x 42,000 tons = 882 lbs or 0.44 tons of PM-10
```

Where actual truck counts/recipts by type of truck are known, then the above calculations can be made directly.

(3) The emission factors for headhouse and internal handling, and bin vents should be applied to the total amount of grain that is handled by these facilities. The headhouse and internal handling emission factor represents dust emissions from bin and basement conveyors, internal cleaners not vented to the atmosphere, scales, garners, legs and distributors.

Example: The facility reports that it handles 50,000 tons of grain. The calculated uncontrolled PM-10 emissions from these operations are:

```
50,000 \text{ tons } \times 0.034 \text{ lbs/ton} = 1,700 \text{ lbs or } 0.85 \text{ tons of PM-}10
```

(4) The emission factor for internal vibrating cleaners is based on emissions from a control device and should be applied only in cases when the emissions are vented to the atmosphere. In cases where the internal cleaner is controlled with a fabric filter, calculated emissions will be biased high and the difference between the control efficiencies of both types of control devices should be accounted for when arriving at the final estimate. In cases where emissions from an internal cleaner are not controlled with a fabric filter or cyclone control device, the headhouse and internal operations emission factor accounts for any internal emissions from equipment within the structure that might escape to the atmosphere.

Example: The facility reports that it cleaned 5,000 tons of grain. The cleaner is aspirated using a cyclone collector and the emissions are vented to the atmosphere. The calculated controlled PM-10 emissions are:

```
5,000 \text{ tons } \times 0.019 \text{ lbs/ton} = 94 \text{ lbs or } .05 \text{ tons of PM-}10
```

(5) The emission factors for column and rack dryers should be applied to the amount of grain dried by the facility. As rack dryers are normally equipped with self-cleaning rotary screens, it would be appropriate to apply the controlled emission factor for the rack dryer to the total amount of grain dried at the facility.

Example: The facility reports drying 10,000 tons of grain using a column dryer. The calculated uncontrolled PM-10 emissions are:

```
10,000 \text{ tons } \times 0.055 \text{ lbs/ton} = 550 \text{ lbs or } 0.28 \text{ tons of PM-}10
```

Example: The facility reports drying 10,000 tons of grain using a rack dryer that is equipped with a self-cleaning rotary screen. The calculated controlled PM-10 emissions are:

```
10,000 \times 0.12 \text{ lbs/ton} = 1,200 \text{ lbs or } 0.60 \text{ tons of PM-}10
```

Example of the application of the emission factors in Table 9.9.1-1 to different types of grain handling operations:

Example 1 (uncontrolled emissions): A country elevator that receives 50,000 tons of grain by truck (80% by hopper and 20% by straight truck) and ships 8,000 tons by truck and 40,000 tons by rail (2,000 tons remain in storage). The facility also dried 10,000 tons of grain using a column dryer and cleaned 40,000 tons with an internal vibrating cleaner controlled by a cyclone cleaner vented to the atmosphere. The 48,000 tons shipped had to be re-elevated for loadout. The grain cleaned also was re-elevated as the grain was dried. Therefore, the grain handled is the grain received, plus that shipped, plus that cleaned, plus that dried. Calculated uncontrolled PM-10 emissions from the facility would be:

## Receiving:

```
(0.8 \times 0.0078 + 0.2 \times 0.059) \times 50,000 \text{ tons} = 900 \text{ lbs or } 0.45 \text{ tons of PM-}10
```

### Shipping:

```
0.029 \times 8,000 \text{ tons} + 0.0022 \times 40,000 \text{ tons} = 320 \text{ lbs or } 0.16 \text{ tons of PM-}10
```

#### Handling/Internal Operations:

```
0.034 \times (50,000 + 48,000 + 40,000 + 10,000) tons = 5,000 lbs or 2.5 tons of PM-10
```

#### Cleaning:

 $0.019 \times 40{,}000 \text{ tons} = 760 \text{ lbs or } 0.38 \text{ tons of PM-}10$ 

#### Drying:

 $0.055 \times 10{,}000 \text{ tons} = 550 \text{ lbs or } 0.28 \text{ tons of PM-}10$ 

Total uncontrolled emissions of PM-10 from the facility would then be the sum of the above emissions or 7,500 lbs or 3.8 tons. To estimate total particulate (PM) emissions, multiply the PM-10

emissions for the facility by 4 so that, for this example, PM emissions would equal approximately 30,000 lbs or 15.2 tons.

Example 2 (controlled emissions): A system (conveying, cleaning, receiving, etc.) is aspirated to a baghouse filter. The facility reports handling 50,000 tons and that the design capacity of the aspiration system is 18,000 cubic feet per minute (cfm). A Method 5 emission test on a comparable system revealed a filter exhaust loading of 0.005 grains per actual cubic foot (gr/acf) of exhaust air and the typical handling rate of the system in question is 350 tons/hour.

The controlled emissions from the system would be calculated as follows:

0.005 gr/acf x 1 lb/7,000 grains x 18,000 acf/min x 60 min/hr x (50,000 tons/year)/(350 tons/hour) = 110 lbs or 0.055 tons of PM.

9.9.1.4 Updates Since the Fifth Edition

The background document (Reference 1) for this section was released in May 1998 with the AP-42 section appearing as part of Supplement D in June 1998. Revisions to Section 9.9.1 since that date are summarized below:

April 2003 -- Emission factors for barge and ship loading/unloading incorporated into Table 9.9.1. Table 9.9.1 expanded to include PM-2.5 emission factors and ratings. Particle size data from Reference 40 used to scale PM-10 emission factors to other particle size ranges. Changes documented in Reference 41. Bin vent emission factor restored from earlier version of Table 9.9.1-1. Additional text revisions for clarification and to reflect current practice in the industry.

Table 9.9.1-1. PARTICULATE EMISSION FACTORS FOR GRAIN ELEVATORS<sup>a</sup>

14010 3.3.1 1	i i i i i i i i i i i i i i i i i i i	Filterable <sup>b</sup>								
			1	Filter	abie	ı				
Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10°	EMISSION FACTOR RATING	PM-2.5 <sup>d</sup>	EMISSION FACTOR RATING			
Grain receiving (SCC 3-02-005-05)										
Straight truck (SCC 3-02-005-51)	None	0.18 <sup>e</sup>	Е	$0.059^{\rm f}$	Е	$0.010^{g}$	Е			
Hopper truck (SCC 3-02-005-52)	None	0.035e	Е	$0.0078^{\rm f}$	Е	0.0013 <sup>g</sup>	Е			
Railcar (SCC 3-02-005-53)	None	$0.032^{\rm f}$	Е	$0.0078^{\rm f}$	Е	0.0013 <sup>g</sup>	Е			
Barge (SCC 3-02-005-54)										
Continuous barge unloader (SCC 3-02-005-56)	None	0.029 <sup>h</sup>	Е	$0.0073^{j}$	Е	0.0019 <sup>j</sup>	Е			
Marine leg (SCC 3-02-005-57)	None	0.15 <sup>h</sup>	Е	$0.038^{j}$	Е	$0.0050^{j}$	Е			
Ships (SCC 3-02-005-55)	None	0.15 <sup>k</sup>	Е	$0.038^{k}$	Е	$0.0050^{k}$	Е			
Grain cleaning (SCC 3-02-005-03)										
Internal vibrating (SCC 3-02-005-37)	Cyclone	$0.075^{m}$	Е	0.019 <sup>n</sup>	Е	$0.0032^{\rm g}$	Е			
Grain drying (SCC 3-02-005-04)										
Column dryer (SCC 3-02-005-27)	None	0.22 <sup>p</sup>	Е	0.055 <sup>n</sup>	Е	$0.0094^{\rm g}$	Е			
Rack dryer (SCC 3-02-005-28)	None	$3.0^{p}$	Е	0.75 <sup>n</sup>	Е	0.13 <sup>g</sup>	Е			
	Self-cleaning screens (<50 mesh)	0.47 <sup>p</sup>	Е	0.12 <sup>n</sup>	Е	$0.020^{g}$	Е			
Headhouse and grain handling (SCC 3-02-005-30) (legs, conveyors, belts, distributor, scale, enclosed cleaners, etc.)	None	0.061 <sup>f</sup>	Е	0.034 <sup>f</sup>	E	0.0058 <sup>g</sup>	E			
Storage bin (vent) (SCC 3-02-005-40)	None	0.025 <sup>q</sup>	Е	0.0063 <sup>n,q</sup>	Е	0.0011 <sup>g,q</sup>	Е			

Table 9.9.1-1 (cont.).

		Filterable <sup>b</sup>							
Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10°	EMISSION FACTOR RATING	PM-2.5 <sup>d</sup>	EMISSION FACTOR RATING		
Grain shipping (SCC 3-02-005-06)									
Truck (unspecified) (SCC 3-02-005-60)	None	0.086e	Е	$0.029^{\rm f}$	Е	$0.0049^{\rm g}$	Е		
Railcar (SCC 3-02-005-63)	None	$0.027^{\rm f}$	Е	$0.0022^{\mathrm{f}}$	Е	$0.00037^{\rm g}$	Е		
Barge (SCC 3-02-005-64)	None	0.016 <sup>h</sup>	Е	$0.0040^{j}$	Е	$0.00055^{j}$	Е		
Ship (SCC 3-02-005-65*)	None	0.048 <sup>h</sup>	Е	$0.012^{j}$	Е	$0.0022^{j}$	E		

- Specific sources of emission factors are cited in Reference 1, Table 4-16 and supporting tables, except as indicated in the following footnotes. Factors are in units of lb/ton of grain handled or processed. Lb/ton divided by 2 gives kg/Mg. SCC = Source Classification Code. ND = no data available. Example uses of emission factors in this table are provided in Section 9.9.1.3.
- <sup>b</sup> Weight of total filterable PM, regardless of size, per unit weight of grain throughput.
- ° Weight of PM ≤ 10 micrometers (µm) in aerodynamic diameter per unit weight of grain throughput.
- <sup>d</sup> Weight of PM ≤ 2.5µm in aerodynamic diameter per unit weight of grain throughput.
- <sup>e</sup> Mean of two values from References 18 and 19.
- f Reference 19.
- <sup>g</sup> Emission factor for PM-10 scaled to PM-2.5 using the mean ratio of 17 percent from Reference 40.
- <sup>h</sup> PM-10 emission factor scaled to total particulate using the ratio of 25 percent presented in Reference 1.
- <sup>j</sup> Reference 40.
- <sup>k</sup> Unloading a vessel with a marine leg is analogous to use of a marine leg in barge unloading.
- <sup>m</sup> Mean of six A- and C-rated data points from References 20, 21, 22, 23, and 24.
- <sup>n</sup> PM-10 emission factor estimated by taking 25 percent of the filterable PM emission factor.
- <sup>p</sup> Mean of two D-rated data points from Reference 2.
- <sup>q</sup> Based on average of wheat and sorghum PM emission factors reported in Reference 42. PM emission factors based on data at the inlet of an aspirated capture/collection system. Due to natural removal processes, uncontrolled emissions may be overestimated compared to those emissions that occur without such a system.

Table 9 9 1-2 PARTICULATE EMISSION FACTORS FOR GRAIN PROCESSING FACILITIES<sup>a</sup>

			Filteral	ble <sup>b</sup>			Conder	nsible PM <sup>c</sup>	
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Animal feed mills Grain receiving (SCC 3-02-008-02)	None	0.017°	Е	0.0025 <sup>e</sup>	Е				
Grain cleaning (SCC 3-02-008-07)	Cyclone	(f)		(f)					
Storage	None	ND		ND					
Grain milling (SCC 3-02-008-15)									
Hammermill	Cyclone	$0.067^{\rm h}$	Е	(g)					
(SCC 3-02-008-17)	Baghouse	$0.012^{j}$	Е	(y)					
Flaker (SCC 3-02-008-18)	Cyclone	0.15 <sup>k</sup>	E	(g)					
Grain cracker (SCC 3-02-008-19)	Cyclone	$0.024^{k}$	E	(g)					
Mixer	None	ND		ND					
Conditioning	None	ND		ND					
Pelletizing Pellet cooler <sup>m</sup> (SCC 3-02-008-16)	Cyclone	0.36 <sup>n</sup>	E	(g)				0.059 <sup>p</sup>	Е
(SCC 3-02-008-10)	High efficiency cyclone <sup>r</sup>	0.15 <sup>q</sup>	Е	(g)					
Feed shipping (SCC 3-02-008-03)	None	0.0033°	Е	0.0008e	E				
Wheat flour mills Grain receiving (SCC 3-02-007-31)	None	(f)		(f)					
Grain handling (SCC 3-02-007-32) (legs, belts, etc.)	None	(f)		(f)					

Table 9.9.1-2 (cont.).

			Filteral	ole <sup>b</sup>		Conder	sible PM <sup>c</sup>		
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Cleaning house separators (SCC 3-02-007-33)	Cyclone	0.012 <sup>s</sup>	Е	(g)					
Wheat milling (SCC 3-02-007-34) (roller mill)	None	$70^{\rm s}$	Е	(g)					
Bulk loading		ND		ND					
Corn dry mills Grain receiving (SCC 3-02-007-41)	None	(f)		(f)					
Grain drying (SCC 3-02-007-42)	None	(f)		(f)					
Grain handling (SCC 3-02-007-43) (legs, belts, etc.)	None	(f)		(f)					
Grain cleaning (SCC 3-02-007-44)	None	(f)		(f)					
Degermer/milling (SCC 3-02-007-45)		ND		ND					
Bulk loading		ND		ND					
Rice Mills Grain receiving (SCC 3-02-007-71)	None	ND		ND					
Precleaning/handling (SCC 3-02-007-72)		ND		ND					
Rice drying (SCC 3-02-007-73)	None	0.063 <sup>t</sup>	Е	(g)					
Cleaning house (SCC 3-02-007-74)		ND		ND					

Table 9.9.1-2 (cont.).

			Filterable <sup>b</sup>				Conder	nsible PM <sup>c</sup>	
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Parboiling	None	ND		ND					
Mill house (SCC 3-02-007-76)	Fabric filter	0.27 <sup>u</sup>	Е	(y)					
Paddy cleaner (SCC 3-02-007-75)	Fabric filter	0.0031 <sup>u</sup>	Е	(y)					
Aspirator (SCC 3-02-007-77)	Fabric filter	0.0030 <sup>u</sup>	E	(y)					
Bran handling (SCC 3-02-007-78)	Fabric filter	0.017 <sup>u</sup>	E	(y)					
Trumbel	None	ND		ND					
Trieurs	None	ND		ND					
Packaging/Shipping		ND		ND					
Durum Mills Grain receiving (SCC 3-02-007-11)		(f)		(f)					
Grain precleaning/ handling (SCC 3-02-007-12)		ND		ND					
Cleaning house (SCC 3-02-007-13)		ND		ND					
Durum milling (SCC 3-02-007-14)		ND		ND					
Bulk loading		ND		ND					

Table 9.9.1-2 (cont.).

			Filteral	ole <sup>b</sup>			Conder	sible PM <sup>c</sup>	
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Rye Mills Grain receiving (SCC 3-02-007-21)		(f)		(f)					
Grain precleaning/ handling (SCC 3-02-007-22)		(f)		(f)					
Cleaning house (SCC 3-02-007-23)		ND		ND					
Rye milling (SCC 3-02-007-24)		ND		ND					
Bulk loading		ND		ND					
Oat Mills (SCC 3-02-007-60)									
Grain receiving		(f)		(f)					
Grain cleaning		(f)		(f)					
Separators		ND		ND					
Drying/cooling		ND		ND					
Grading/sizing		ND		ND					
Hulling		ND		ND					
Cutting		ND		ND					
Steaming/conditioning		ND		ND					
Flaking		ND		ND					
Screening		ND		ND					
Packaging		ND		ND					

Table 9.9.1-2 (cont.).

			Condensible PM <sup>c</sup>						
Type of Facility/ Emission Source	Type of Control	PM	EMISSION FACTOR RATING	PM-10 <sup>d</sup>	EMISSION FACTOR RATING	Inorganic	Organic	Total	EMISSION FACTOR RATING
Barley Malting Grain receiving (SCC 3-02-007-08)	Fabric filter	0.016 <sup>v</sup>	E	(y)					
Gas-fired malt kiln (SCC 3-02-007-09)	None	0.19 <sup>w</sup>	Е	0.17 <sup>x</sup> (PM-2.5 =0.075)	Е	0.075 <sup>x</sup>	0.013 <sup>x</sup>	0.088 <sup>x</sup>	Е

- Specific sources of emission factors are cited in Reference 1, Table 4-17 and supporting tables. Factors are in unit of lb/ton of grain handled or processed. Lb/ton divided by 2 gives kg/Mg. SCC = Source Classification Code. ND = no data available.
- Weight of total filterable PM, regardless of size, per unit weight of grain throughput.
   Condensible PM is material collected in the impinger portion of a PM sampling train.
- d Weight of PM ≤ 10μm in aerodynamic diameter per unit weight of grain throughput.
- <sup>e</sup> Reference 38. Feed shipping emission factor based on data for loading of bulk feed (not pellets).
- f See emission factors for grain elevators, Table 9.9.1-1.
  g PM-10 test data are not available. PM-10 emission factors can be estimated by taking 50 percent of the filterable PM emission factor.
- Mean of two values from References 26 and 27.
- <sup>j</sup> Mean of two B-rated values from References 28, 29, and 30.
- <sup>k</sup> Reference 31.
- <sup>m</sup> Includes column and pan dryers.
- <sup>n</sup> Mean of 11 A-, B-, and C-rated values from References 26, 27, 31, and 32.
- <sup>p</sup> Mean of three B- and C-rated values from References 26 and 32.
- <sup>q</sup> Mean of two B-rated values from References 29, 30, and 31.
- <sup>r</sup> Equivalent to triple cycle or modern high efficiency cyclone.
- s Reference 2.
- <sup>t</sup> Mean of five D-rated values from Reference 34.
- <sup>u</sup> Reference 35.
- v Reference 36.
- w Mean of two values from References 36 and 37. Value converted from bushels to tons using a conversion factor of 50 bu/ton.
- x Reference 37.
- <sup>y</sup> PM-10 test data are not available. PM-10 emission factors can be estimated by taking 100 percent of the filterable PM emission factor.

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# FIGURE 1

**LOCATION MAP** 

